LIGAND BRIDGING IN THE OXIDATION OF CHROMIUM(II) AT MERCURY ELECTRODES

Thesis by
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1967

Dedicated to
Thomas Armstrong Peebles
1882-1965

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ABSTRACT

Controlled potential electrolysis and electrochemical relaxation techniques have been used to investigate the mechanism of oxidation of chromium(II) at mercury electrodes in the presence of chloride, bromide, and iodide. It is shown that the major path for the oxidation is through a bridged activated complex of the type Hg--X--Cr.

Kinetic parameters have been determined for the bromide-dependent path and the halide-independent path. Equations have been derived to predict from kinetic data the product distribution between two competing reactions.

It is suggested that the activated complex is formed with halide adsorbed on the electrode surface.

The limitations of chronopotentiometry at hanging mercury drop electrodes have been investigated and corrections are given for spherical diffusion effects at times greater than 0.1 sec. It is demonstrated that reverse current chronopotentiometry under these conditions is a qualitatively unreliable technique.

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PART I

GENERAL INTRODUCTION

Chapter 1

INTRODUCTION

As early as 1947 Heyrovsky (1) suggested that the accelerating effect of halide ions on the irreversible reduction of many metal ions at mercury electrodes is due to the ability of adsorbed halide to act as an efficient bridge for electron transfer. The vigor with which research is presently being carried on in the area of ligand bridging both in homogeneous solution and electrode reactions is an appropriate comment on Heyrovsky's insight. This thesis is concerned with the study of the role of bridging ligands in the oxidation of Cr(II) at mercury electrodes.

The basic ideas of the bridging mechanism in homogeneous reactions are well known (2) and do not need further discussion here. The extension to heterogeneous reactions is less generally known and deserves some comment.

Halides with the exception of fluoride are strongly adsorbed on mercury electrodes at potentials anodic to the null charge potential. The basic idea of the extension of the concept of ligand bridging to electrode reactions is to consider the combination of electrode and adsorbed ligand as analogous to a metal ion-ligand complex, and then to draw the parallel between the homogeneous reaction

$$MX^{+n} + *M^{+m} \longrightarrow (MX^*M)^{+n+m}$$
 (1)

and the heterogeneous reaction

$$Hg(X)_{ads} + M^{+n} \longrightarrow Hg(XM^{+n})_{ads}$$
 (2)

where the products in (1) and (2) are the reactive intermediates or transition states for the electron transfer reactions.

If one wishes to study reactions of the type

$$Hg(X^{-})_{ads} + M^{+n} \xrightarrow{-e^{-}} MX^{+n}$$
 (3)

the use of Cr(II) as M⁺ⁿ is particularly attractive. When X is chloride, the supposed product of the reaction, CrCl²⁺, * though thermodynamically unstable, is sufficiently substitution inert that solutions of CrCl²⁺ can be titrated with silver ion without appreciable decomposition of the complex. This provides a substantial simplification of the problem of product analysis.

A second reason for the choice of Cr(II) for the study of ligand bridging in electrochemical reactions is that it is oxidized in the range 0 to -0.5 v. vs. SCE, the potential range of major interest for mechanisms involving halide adsorption.

An ancillary factor favoring the choice of Cr(II) is the large amount of work that has been done on the role of ligand bridging in the homogeneous oxidation of Cr(II) (3); this work serves as a guide and comparison for electrochemical studies.

^{*}For simplicity coordinated water molecules will not be included in complex ion formulas. The formula ${\rm CrCl}^{2^+}$, for instance, is intended to imply the complex ion ${\rm Cr}({\rm H}_2{\rm O})_5{\rm Cl}^{2^+}$.

It has been shown that many ligands dramatically affect the electrochemical oxidation of Cr(II). Pecsok and Lingane (4) have investigated the polarographic behavior of Cr(II) in the presence of KCl, KSCN, CaCl₂, Me₄NBr, and several carboxylic acids. Large changes in apparent half-wave potential and in the degree of irreversibility of the oxidation were found by changing the nature of the supporting electrolyte solution.

Kemula and Rakowska (5), who studied the reduction of various Cr(III) species using cyclic voltammetry, present some interesting qualitative results. They found that when Cr^{o^+} is reduced in chloride solutions, on the second cycle of cathodic polarization a second peak appears anodic to the peak initially observed for the reduction of $Cr^{ooldsymbol{3}}$. As the concentration of chloride in the supporting electrolyte solution is increased, this peak becomes larger and more clearly separated from the $Cr^{ooldsymbol{3}}$ peak. The potential at which this peak occurs is the same as that for the reduction of $CrCl^{ooldsymbol{2}}$ obtained from the salt $CrCl_{ooldsymbol{3}}$.

Aikens and Ross (6) have studied the rates of oxidation of Cr(II) at mercury electrodes in the presence of fluoride, chloride, and iodide. They found that the rate of Cr(II) oxidation is proportional to the concentration of chloride over a fifty-fold change in chloride concentration, and that at a fixed potential, the accelerating effect of the halides decreases in the order $(I^-) > (Cl^-) \gg (F^-)$, the effect of fluoride being very small. They point out that the tendency for specific adsorption of halides also decreases in this order, while the stability of the Cr(II) halides probably increases markedly in the same order.

It has not been understood how halides increase the rate of oxidation of Cr(II) at mercury electrodes. In the case of chloride we have a model system which gives us an opportunity to identify unambiguously gross features of the mechanism. Cr(III) is sufficiently inert to chloride substitution that the reaction

$$Cr^{3^{+}} + Cl^{-} \longrightarrow CrCl^{2^{+}}$$
 (4)

may be ignored as a source of the complex $\operatorname{CrCl}^{2^+}$. Therefore if the product of electro-oxidation of $\operatorname{Cr}(\operatorname{II})$ in chloride solutions is $\operatorname{CrCl}^{2^+}$ the transition state must contain chloride. But since the tendency for CrCl^+ formation is very small (7) this implies that the chloride in the transition state is intimately involved in the mechanism. The only way for this to be true is for the chloride to be bound to the chromium and also to interact strongly with the electrode surface. The only plausible coherent mechanism with these characteristics is that of halide bridged electron transfer. If the product of electro-oxidation of $\operatorname{Cr}(\operatorname{II})$ in chloride solutions is found to be $\operatorname{CrCl}^{2^+}$ the bridge mechanism is established and any arguments about a more detailed description of the mechanism do not change or challenge the validity of this conclusion. Chapters 3-6 of this thesis present experimental results which imply the bridge mechanism.

When it has been shown that the bridged transition state or intermediate is necessary to the mechanism, the question arises of how the bridged state is formed. The reaction may proceed primarily through the complex CrCl⁺; alternatively the key to the mechanism may be found in considering the analogy between halide adsorbed on a mercury surface

and halide in a complex oxidizing agent. From the latter viewpoint, the reaction can best be explained by electron transfer to the electrode from chromium via the chloride bridge. This proposed mechanism is quite general and may be used to explain a wide variety of electrochemical reactions.

The simplicity of this idea is not matched by its susceptibility to experimental verification. The difficulty lies in the large non-specific effects which the halides have on irreversible reactions due to the effect of their adsorption on the structure of the electric double layer (8). A priori descriptions of the nature of the double layer in the presence of specifically adsorbed ions are not yet available, and very little data of adequate quality has been obtained to attack this problem. Also, the nature and extent of the adsorption itself is incompletely understood.

This means that any progress in understanding the details of the bridge state formation must rest on the patient accumulation and comparison of data on the oxidation of Cr(II) under a variety of conditions. It seems unlikely that so complex a system can be made to yield its secrets with a few cleverly designed experiments.

Chapter 7 of this thesis presents more detailed arguments about the nature of the bridging mechanism with supporting experimental evidence.

Chapter 2

EXPERIMENTAL CONSIDERATIONS

During the course of this work the procedures and apparatus directly concerned with Cr(II) solutions have been successively and somewhat successfully modified to give better results than did the original designs. As an aid to the interested experimenter this material is collected here together with some pertinent comments on chromium chemistry.

I. The Preparation of Chromium(II) Solutions

The most satisfactory general method of preparing Cr(II) solutions is by electrolysis of Cr(III) solutions at a mercury cathode. The Cr(III) solution for electrolysis is prepared by hydrogen peroxide reduction of a perchloric acid solution of sodium dichromate followed by heating in the presence of platinized platinum to decompose the excess peroxide. The resulting solution has the characteristic violet color of Cr3⁺.

Stock solutions 0.2 F in Cr(III) and 2 F in $HClO_4$ were prepared in this manner. Solutions for electrolysis were 300 ml. of Cr(III) stock solution diluted 1:1 with water. The resulting Cr(II) solutions typically were 0.09 F in Cr(II), 1.0 F in $HClO_4$ ($\mu = 1.5$).

The electrolysis is carried out in the three compartment cell shown in Figure 1. A continuous flow of 1 F HClO₄ is maintained through the center compartment throughout the course of the electrolysis to completely isolate the cathode compartment from the anode compartment. The

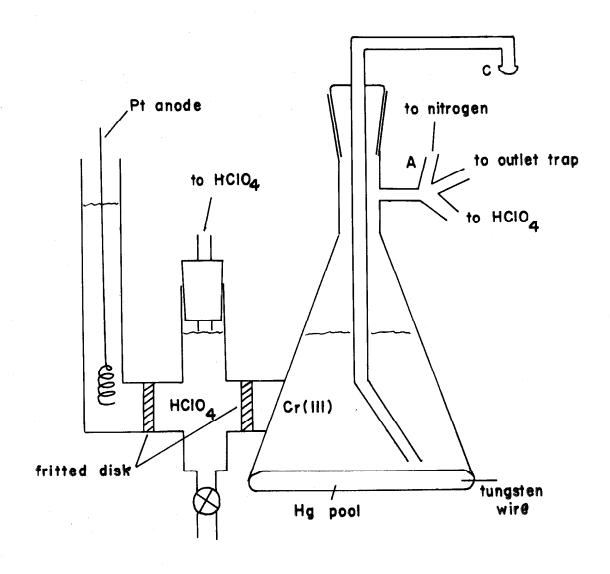


Figure 1. Electrolysis cell for preparing Cr(II) solutions.

electrolysis is carried out by applying 12 v. between the platinum wire anode and the stirred mercury pool cathode. The back EMF of the cell is about 2 v. The current is 0.8 - 1.0 amp. The electrode area is about 135 cm.² Under these conditions the reduction takes place with copious hydrogen evolution; the current efficiency is 50-70%.

The flow of perchloric acid through the center compartment helps to maintain the hydrogen ion concentration in the cathode compartment and thus prevent precipitation of Cr(OH)₂ which would ruin the preparation.

The electrolysis is carried out under positive nitrogen pressure as indicated by the difference in solution levels between the center and anode compartments. The pressure in the center and cathode compartments is equalized by connecting the HClO₄ reservoir and the cathode compartment to the outlet trap. The perchloric acid flow is maintained by siphon.

The outlet trap consists of successive flasks containing V(II) in 1 F H₂SO₄ and water, respectively. The V(II) is kept in the reduced state by zinc amalgam. The back-diffusion of oxygen into the system even with high nitrogen flow rates and very long outlet tubes is sufficiently large that a trap is an absolute necessity.

The nitrogen flow through the system is maintained by a nitrogen inlet at D to the Cr(II) reservoir (Figure 2), which is connected to the cell at C. The reservoir is initially purged of oxygen by repeatedly evacuating and filling with nitrogen.

When the electrolysis appears to be finished, the Cr(II) solution is transferred to the reservoir by closing off all the cell openings

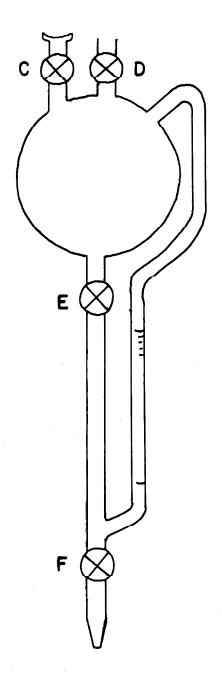


Figure 2. Storage buret for Cr(II) solutions.

(including the center and anode compartments), shunting the nitrogen flow from the reservoir (D) to the cell inlet at A, and forcing the solution over into the reservoir. Since it is most convenient to carry out this transfer with small pressure differences, during the transfer a loak to vacuum is made through F with D and E closed (Figure 2). When the transfer has been completed C and F are closed, and nitrogen is introduced at D until the pressure in the reservoir is about two atmospheres absolute (the volume of the solution is about half the volume of the reservoir).

The standard taper joint below F (Figure 2) is fitted with an adapter for transfer of solution. The adapter is a 15 cm. length of 1 mm. capillary tubing with a matching standard taper joint at the top and a 12/1 ball joint at the bottom for flexibility. The dead space below the stopcock F is filled with small glass beads to decrease the loss of Cr(II) by air oxidation in the interval while connection of the reservoir to the receiver is made.

The stopcocks in the reservoir may be Teflon (4 mm. bore), which leak, or precision ground pressure stopcocks, which contaminate the solution with grease. Both are tolerable, neither is satisfactory.

Chromium(II) solutions can also be prepared by oxidizing the metal with acid. "Spectrographically Standardized Chromium Pellets" available from Johnson, Matthey, and Co., Ltd. (73/83, Hatton Garden, London E.C. 1) was found to be the most satisfactory source of chromium metal. This reaction is smooth and rapid in dilute HCl, but will not start in HClO₄ unless the metal is first activated by dipping in HCl. If the metal is then washed and placed in dilute (2 F) HClO₄ solution

the reaction proceeds at a lively pace for some time, but eventually the surface of the metal darkens and the rate of reaction decays to zero. This method of preparation is useful for making small amounts of dilute Cr(II) solutions, particularly if chloride is present, but seems not generally suitable for the preparation of stock solutions.

If the presence of zinc can be tolerated Cr(II) solutions are also readily prepared by reduction of Cr(III) solutions in a Jones reductor. The zinc amalgam must be light and must be pretreated with warm acid to ensure quantitative reduction of the Cr(III) (9). The solution is best transferred directly into the oxygen-free reservoir and then put under nitrogen pressure, as described above.

Nitrogen, free of oxidizing impurities, is most conveniently obtained by passing Matheson "prepurified" nitrogen over hot copper turnings. A Vycor tube filled with copper turnings and a tube furnace for this purpose are available from E. H. Sargent and Co. The nitrogen is then cooled and presaturated by passing it through a washing tower filled with the appropriate solution.

The large oxygen leakage through Tygon or equivalent tubing makes it unsuitable for use. A thick wall synthetic rubber tubing, e.g., chlorinated butyl tubing, is recommended. Good rubber to glass seals can be made with Apiezon Q wax.

II. Analysis of Chromium(II) Solutions

Chromium(II) stock solutions were analyzed for Cr(II) by adding 10 ml. of the solution to 100 ml. of deaerated Fe(III) solution (prepared by adding 58 g. of Fe₂(SO₄)₃·(NH₄)₂SO₄·24H₂O to 50 ml. of 18 F H₂SO₄ plus 80 ml. of 85% H₃PO₄ and diluting to 2 l.). The resulting solution was then titrated with approximately 0.02 N Na₂Cr₂O₇ to a visual endpoint using 6 drops of sodium diphenylamine sulphonate indicator. The titration requires some practice because the bright green color of Cr(III) obscures the color change at the endpoint. The blank is negligible.

The Cr(II) solutions were analyzed for total chromium by adding 2 ml. of the solution to 14 ml. of 1 F NaOH plus a few drops of 30% $\rm H_2O_2$, boiling to decompose excess peroxide, diluting to 1 l. and comparing the absorbance at 373 mm. with that of a standard solution differing in absorbance by less than 5%. The molar absorptivity of chromate at 373 mm. is 4760 (10).

These procedures have the advantage that the same $Na_2Cr_2O_7$ standard solution can be used for preparation and both analyses of the Cr(II) stock solution.

The solutions were analyzed for hydrogen ion by adding 2 ml. of the solution to 50 ml. of deaerated solution containing 0.2 g. of ethylene diamine dihydrochloride and titrating potentiometrically with 0.1 F NaOH solution under air-free conditions using glass and NaCl-SCE electrodes. The pH at the endpoint is the same as that of the original ethylene diamine dihydrochloride solution.

Carbonate-free O.1 F NaOH solutions were prepared by diluting 6 ml. of saturated NaOH solution to 1 l. with freshly boiled and cooled water and standardizing against potassium hydrogen phthalate using a potentiometric endpoint.

III. Oxidation-Reduction Reactions of Cr(II) and Cr(III)

1. The Oxidation of Cr(II) and Cr(III) by Perchlorate.

The quantitative exidation of chromium to Cr(VI) by boiling in concentrated HClO₄ is part of a well known standard procedure for chromium determination. In 2 F HClO₄ this reaction occurs to a small extent even on mild heating. The practice of refluxing with excess silver ion to decompose CrCl²⁺ (ll) should not be indiscriminately applied.

Analysis of a Cr(II) stock solution at intervals of one or two weeks gave a ratio of the drop in titer to the chloride concentration of 6 to 7 corresponding roughly to the reduction of perchlorate to chloride by Cr(II). The chloride-free life of the solutions was found to be a month to six weeks.

2. The Oxidation of Cr(II) by Nitrate in Acid Solution.

In this work NaClO₄ was used as the innocuous salt to maintain constant ionic strength. This introduces a deceptively simple problem which arises from the limited solubility of KClO₄. A standard commercial SCE reference electrode cannot be used in a NaClO₄ solution because KClO₄ precipitates in the junction. One approach used to avoid this problem was to place the electrode in a salt bridge containing 1 F NaNO₃ solution. The junction between the NaNO₃ solution and the NaClO₄ solution

was a cracked glass bead. The NaNO3 solution isolates the cell from the chloride in the electrode and isolates the electrode from perchlorate in the cell.

The difficulty with this arrangement is that the leak rate of solution from the salt bridge into the cell, even with cracks having a resistance of 20 k Ω or larger, is great enough to introduce large amounts of nitrate into the cell in the course of an experiment. It was found that in acid solution nitrate (or nitric acid) rapidly oxidizes Cr(II), probably to $\text{CrNO}_2^{2^+}$.

Figure 3 shows the spectrum of a solution of Cr(II) in 0.1 F HClO₄, 0.9 F NaClO₄ to which had been added sufficient NaNO₃ to completely oxidize the Cr(II) to Cr(III). The spectrum labeled 1 was taken almost immediately after the addition of nitrate, the second 3 hours later, and the third 20 hours later. The broad peak at 430 mm. in 1 is characteristic of Cr(III) but does not correspond to the species Cr³⁺ which has peaks at 407 and 575 mm. (2). In 2 and 3 this peak moves toward shorter wavelengths. At the same time sharp peaks appear at 358, 370, and 387 mm. Bunton and Stedman (12) report peaks for HNO₂ at 356, 369, and 383 mm.

On standing for several days, the oxidation product solution, which initially was golden yellow, had changed to the characteristic violet color of ${\rm Cr}^{3^+}$.

These observations indicate that HNO_3 oxidizes Cr(II) to $CrNO_2^{2^+}$ in acid, and that the product slowly dissociates to form Cr^{2^+} and HNO_2 .

When Cr(II) is oxidized by nitrate in the presence of bromide, the product solution apparently contains a mixture of $CrBr^{2+}$, $CrNO_2^{2+}$,

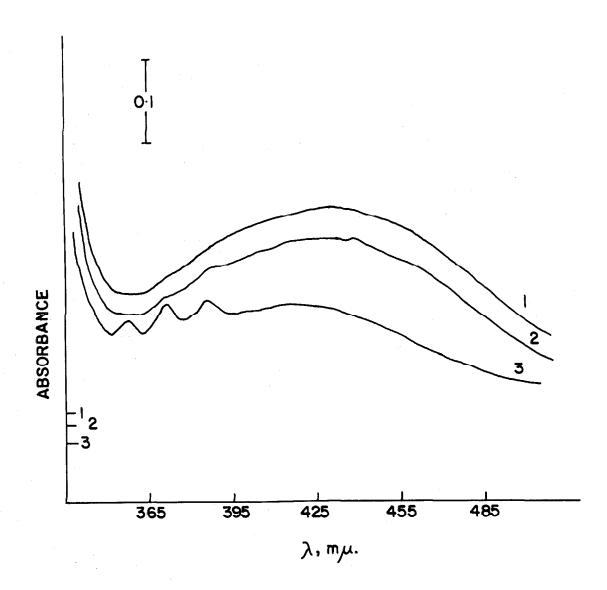


Figure 3. The absorbance of a solution formed by adding 10 ml. of Cr(II) stock solution to 140 ml. of 0.1F HClO₄, 0.9F NaClO₄ and 10 ml. 0.1F NaNO₃. Curve 1:t = 20 min.; curve 2: t = 3 hr.; curve 3: t = 20 hrs. The ordinates 1, 2, 3 are the absorbance zeros.

Cr³⁺, and possibly some dimeric Cr(III) species. 3.6 mF Cr(II) in 0.908 F NaBr, 0.066 F HClO₄ with just sufficient NaNO₃ solution present to cause complete oxidation gave a yellowish-green solution. This solution had a spectrum with peaks at 422 and 575 mµ. in contrast with the values of 407 and 575 mµ. for Cr³⁺ and 432 and 622 mµ. for CrBr²⁺ (2). Cathodic polarography in this solution gave a double wave with the first half-wave potential at about -0.510 v. vs. SCE and the second at about -0.850 v. vs. SCE. The yellowish color indicates that CrNO₂²⁺ is a major product of the oxidation, while the two half-wave potentials correspond to the reduction of CrBr²⁺ and Cr³⁺, respectively. It is suspected that the reduction potential for CrNO₂²⁺ is very near to that of the bromide complex.

It is quite clear that in any work with Cr(II) solutions, nitrate must be rigorously excluded. This point is worth strong emphasis because of the ubiquitous use of NaNO₃ solutions as innocuous or inert salt solutions.

IV. The Rates of Aquation of Halide Complexes of Cr(III)

The choice of technique for the study of the products of the electrochemical oxidation of Cr(II) in the presence of various ligands depends on the lifetime of those products in the solution. Guthrie and King (13) and Swaddle and King (14) have made a thorough study of the rates of aquation of the halide complexes CrX²⁺ as a function of hydrogen ion concentration. Some of their results are presented in Table 1 along with the time required for 1% of the complex to dissociate.

All of these rates are based on spectrophotometric measurements.

TABLE 1

Complex	(H ⁺), M	T, ~C	k, sec. ⁻¹	to.01
CrF ²⁺	0.01	25	7.6×10^{-10}	5.1 months
CrCl ²⁺	2.0	25	2.9 x 10 ⁻⁷	9.6 hours
CrBr ²⁺	1.0	30	1.0 x 10 ⁻⁵	16 minutes
CrI ²⁺	2.0	25	8.6 x 10 ⁻⁵	1.9 minutes

1. The Rate of Aquation of CrCl2+.

We have measured the rate of aquation of the complex CrCl^{2^+} by determining the chloride concentration of a solution of CrCl^{2^+} as a function of time. Chloride concentration was determined in a solution initially 20 mF in CrCl^{2^+} and 2 F in HClO_4 by titrating aliquots of the solution with standard AgClO_4 solution using a potentiometric endpoint with glass and silver wire electrodes.

The pseudo first order rate constant for the dissociation was found to be 3.2 x 10^{-5} min. or the 1% life is 5.2 hours. The temperature was not controlled but was 27.0 \pm 0.2 °C.

2. The Rate of Aquation of CrBr2+.

We have determined the rate of aquation of the complex $\operatorname{CrBr}^{2^+}$ spectrophotometrically. The molar absorptivities of Cr^{3^+} and $\operatorname{CrBr}^{2^+}$ in the visible region of the spectrum are known from the work of King (15) and Taube and Myers (2), respectively. It has been observed by many workers (16) in chromium chemistry that the range 380-500 mm. does not give reliable spectra for concentration measurements because of the high absorptivity of several other chromium species which are likely to be in

the solution in more than trace amounts. Accordingly the concentrations of the two major species in the solution were calculated from the molar absorptivities at two points outside this region, namely 580 and 650 mm. at which the molar absorptivities of Cr^{3^+} are 13.5 and 3.78 and those of Cr^{2^+} 14.0 and 17.1, respectively.

The results are presented in Table 2. The value of k, the pseudo first order rate constant for the dissociation, was found to be 1.79×10^{-4} min.⁻¹, or the complex has a 1% life of 56 minutes.

t-to, min.	A ₆₅₀	A ₅₈₀	(CrBr ²⁺), mM	(Cr(III)), mM
152	0.379	0.350	21.4	25.1
223	0.370	0.350	20.7	25.1
338	0.370	0.347	20.7	25.1
1367	0.331	0.345	17.8	25.0
2530	0.276	0.343	13.7	24.9
3998	0.234	0.336	10.6	24.6

TABLE 2

Experimental details. One ml. of bromine was added to 50 ml. of deaerated 1 F HClO₄ solution, and 17 ml. of 0.1024 F Cr(II) stock solution was added to the mixture. Under these conditions the reaction

$$\operatorname{Cr}^{2^{+}} + \operatorname{Br}_{2} \longrightarrow \operatorname{CrBr}^{2^{+}} + \operatorname{Br}^{-} \tag{1}$$

is quantitative. The reaction mixture was purged of excess bromine by vigorously bubbling nitrogen through the mixture. The composition of the resulting solution was 25.6 mF Cr(III), 1.01 F HClO₄ (μ = 1.12).

The spectrum of this solution was determined as a function of time using a Cary Model 15 recording spectrophotometer.

3. The Effect of Cr(II) on the Rate of Aquation of CrBr2+.

The rate of aquation of CrBr2+ was also measured in the presence of excess Cr(II) to see if Cr(II) catalyzes the aquation reaction.

A seven point equation was used to calculate the concentrations of Cr(II), $CrBr^{2+}$, and Cr^{3+} at each time using the measured absorbance at each wave length and the molar absorptivities given in Table 3.

TABLE 3

	Mola	r Absorptivity	
λ, mμ.	CrBr ²⁺ (15)	Cr ³⁺ (2)	Cr(II)
380	5.7	10.01	0.036
450	19.4	6.64	0.25
540	6.0	9.78	0.93
575	13.0	13.9	0.16
580	14.0	13.5	0.19
590	16.1	12.6	2.26
650	17.1	3.78	4.34

The method of calculation was a simple least squares treatment with the constraint that the total chromium concentration be 30.73 mF. The pseudo first order rate constant for the dissociation of $CrBr^{2+}$ in the presence of Cr(II) was found to be $k=2.20\times 10^{-4}$ min. $^{-1}$, or the 1% life is 46 minutes.

In view of the quality of the data and the known pitfalls in the calculation of Cr(III) complex concentrations in chromium solutions from absorbance data, this result indicates that Cr(II) does not catalyze the rate of dissociation of CrBr²⁺.

Experimental details. The cell used was specifically designed for mixing and transferring air sensitive solutions to spectrophotometer cells by W. P. Schaefer and has been described by him (17).

A chlorine-free saturated aqueous bromine solution was prepared by adding a large excess of bromine to triply distilled water and bubbling nitrogen through the solution for several days. The solubility of bromine in water at 25° C. is 0.210 M (18).

To 50 ml. of oxygen-free 1 F HClO₄ was added under oxygen-free conditions 20 ml. of a Cr(II) stock solution whose composition was 0.0970 M Cr(II), 0.0095 M Cr(III), and 1.093 M HClO₄ (μ = 1.55). A sample was taken from the cell and the visible spectrum of the solution obtained to find the molar absorptivities of Cr(II). Over the range of interest, 380-650 m μ ., the maximum absorbance for Cr(II) occurs at 650 m μ . (ϵ = 4.34). A maximum is found at 410 m μ . (ϵ = 0.93).

To the remaining solution in the cell was added 3 ml. of the saturated bromine solution. These conditions provide approximately a two-fold excess of Cr(II). An aliquot of the resulting solution was analyzed for total chromium by oxidation to chromate as described above (p. 13). The total chromium concentration was found to be 30.7_3 mF. The solution also had $HClO_4 = 1.00$ M ($\mu = 1.12$).

4. Polarographic Determination of the Rate of Aquation of CrBr²⁺.

The diffusion current of a solution containing ${\rm CrBr}^{2^+}$ was measured at -0.610 v. vs. SCE for a period of five hours. Semi-logarithmic plots of diffusion current as a function of time were made for data obtained over intervals of 30 min. at times 100, 220, and 260 minutes. The values of the pseudo first order rate constant for the dissociation of the complex obtained from the slopes were 1.78, 1.21, and 1.65 x 10^{-3} min. $^{-1}$, respectively. The average value is $1.55 \pm 0.22 \times 10^{-3}$ min. $^{-1}$ or the 1% life is 6.5 minutes.

Experimental details. The experiment was done in the cell shown in Figure 18. Sufficient mercury was added to the cell to cover the bottom, and then sufficient saturated NaBr solution to cover the mercury to a depth of about 1 cm. A small amount of solid NaBr was added to insure saturation during the course of the experiment. 140 ml. of deaerated 1 F HClO₄ was carefully floated on top of the saturated NaBr solution, and the cell closed. To this was added 10 ml. of a Cr(II) stock solution 0.095 F in Cr(II), 1.09 F in HClO₄ (μ = 1.55). Finally 0.9 ml. of bromine was added.

The design of the experiment accomplishes several purposes. First, it provides a large and stable combination reference and auxiliary electrode of known potential (-0.160 v. vs. SCE) making possible the use of a conventional commercial polarograph. This would not be possible even in the presence of bromide if the mercury of the pool were not isolated from the Cr(II) solution. Second, it isolated the solution

under investigation from the possible catalytic effect of mercury. The density of the saturated NaBr solution is sufficiently high (1.54 gm./ml.) that there is very little mixing of the two solutions (18).

The diffusion current constant for the reduction of $CrBr^{2+}$ in 1 F HClO₄ was assumed to be 1.54 (19). The drop time was 3.64 seconds and the drop weight 2.52 mg., giving $m^{2/3}t^{1/6}=2.24$. No correction was made for the background current since the measured current was always greater than 12 μa . and any correction would be small.

The same experiment was repeated in the absence of Cr(II). The composition of the solution was 0.147 F HClO₄ and 0.843 F NaBr (μ = 1.02). The initial concentration of CrBr²⁺ was 6.7 mF. The current was recorded over a period of four hours. The rate was found to decrease slowly with time. The initial rate constant was found to be 8.21 x 10^{-3} min.⁻¹.

5. Discussion.

The work of King and co-workers on the aquation of the monohalide complexes of Cr(III) was carefully done for the purpose of obtaining thermodynamic quantities. The rate determinations we have carried out were done before King's values were published and were done to obtain order of magnitude upper limits for the rate constants under conditions comparable to those of our electrochemical experiments. Under the circumstances the agreement with the results of King is good.

However, it should be pointed out the rates measured by spectrophotometric techniques are closer to the values of King than the rates measured by other techniques. In particular, the abnormally high value for the rate of aquation of CrBr²⁺ determined polarographically seems to be outside the limits of expected error, especially since all sources of error would tend to make the apparent rate of decomposition smaller rather than greater.

Resolution of this difference in rate constant might prove to be of fundamental interest. At worst it could lay valuable groundwork for the application of electrochemical techniques to the measurement of bulk concentrations of Cr(II) and Cr(III) species for use in the study of homogeneous reactions of chromium.

The general unreliability of the spectrophotometric techniques now universally used for that purpose should provide a powerful stimulus for development of adequate electrochemical techniques.

PART II

EVIDENCE FOR THE LIGAND BRIDGING MECHANISM

Chapter 3

CONTROLLED POTENTIAL OXIDATION OF CHROMIUM(II) IN THE PRESENCE OF CHLORIDE

Large scale controlled potential electrolyses of Cr(II) solutions were carried out at a stirred mercury pool electrode at -0.012 v. vs. SCE in the presence of chloride. Current-voltage curves showed that the oxidation of Cr(II) in the absence of chloride is diffusion limited at that potential. The amount of Cr(II) oxidized to Cr(III) was determined by integration of the current. The amount of free chloride present in the solution at the conclusion of the electrolysis was determined by titration with silver. The difference between chloride found and chloride initially present gives the amount of CrCl²⁺ in the product.

According to our prediction that the ligand bridging mechanism obtains under the conditions of these experiments the expected result is that when the initial chloride to Cr(II) ratio is less than or equal to one no free chloride will be found in the product solution and when the initial chloride to Cr(II) ratio is greater than one the amount of chloride found will be equal to the initial excess of chloride over Cr(II).

This behavior is illustrated by the solid line in Figure 4. The experimental results are presented in the same figure. The prediction that the oxidation proceeds via ligand bridging is clearly confirmed.

Experimental procedures. Reagent grade chemicals and tap distilled water were used unless otherwise specified.

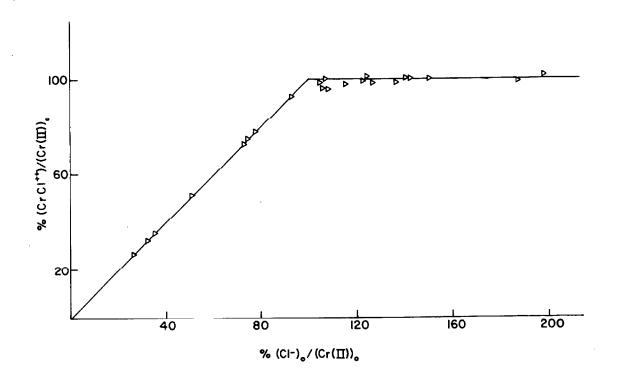


Figure 4. The controlled potential oxidation of $\mathrm{Cr}(\Pi)$ in chloride solutions. $\left(\mathrm{Cr}(\Pi)\right)_0$ and $\left(\mathrm{Cl}^-\right)_0$ are initial concentrations and $\left(\mathrm{Cr}\mathrm{Cl}^{2^+}\right)$ the final concentration of that species. The solid line shows the expected behavior.

Sodium chloride was purified by precipitation from NaCl solution with HCl gas liberated from 12 F HCl by slowly adding 18 F H₂SO₄.

Silver perchlorate solutions were prepared by dissolving G. F. Smith Silver Perchlorate in 2 F HClO₄ and filtering cff the precipitate. They were standardized by titrating samples of a standard NaCl solution potentiometrically using glass and silver wire electrodes. Satisfactory potential response was obtained if the silver wire indicator electrode was cleaned with 12 F HNO₃ containing a pinch of NaNO₂ just before the titration.

Mercury was Mallinckrodt distilled quality. After use in an electrolysis it was repurified by filtering, vigorously bubbling air through the mercury under 10% HNO₃ with glass wool present, and refiltering. It was then used again.

CIT nitrogen was purified by passing through successive gas washing towers containing 0.1 F V(II) in 1 F H_2SO_4 , 0.1 F Cr(II) in 1 F H_2SO_4 , and water. The V(II) and Cr(II) solutions were maintained in the reduced state by zinc amalgam.

Chromium(II) stock solutions approximately 0.1 F in Cr(II) and 2 F in HClO₄ were prepared by reduction of Cr(III) perchlorate solutions in a Jones reductor and were dispensed from a storage buret as described in Chapter 2.

The stock solutions were analyzed for Cr(II) as described in Chapter 2 with the exception that the titration was done with KMnO₄ rather than with Na₂Cr₂O₇ solution. The former gives an obscure but satisfactory visual endpoint due to the color of excess permanganate. The endpoint fades rapidly. The point at which the color persists for

one minute is taken to be the end point. The blank correction is typically 0.3%.

The cell in which the electrolyses were carried out is shown in Figure 5.

The oxidations were carried out at -0.012 v. vs. SCE using an Analytical Instruments, Inc. potentiostat. The number of equivalents of Cr(II) oxidized was determined by an Analytical Instruments, Inc. current integrator in series with the cell.

The electrolysis was carried out in the following manner.

Forty ml. of a solution of NaCl of the desired concentration in 2 F HClO₄ was added to the center compartment of the cell and the same solution with Cr(II) added to prevent diffusion of oxygen into the center compartment through the fritted glass disk connections was added to the reference and auxiliary electrode compartments. The main compartment was then thoroughly purged of oxygen with purified nitrogen before adding 10 ml. of 0.1 F Cr(II) solution from the storage buret. The electrolysis was then begun. The reference electrode was a NaCl-SCE and the auxiliary electrode platinum.

Chloride analyses were done by potentiometric titration with AgClO₄ solution 2 F in HClO₄ using glass and silver wire electrodes. The titrations were done at room temperature in dim light. Titrations done at 0° C. with exclusion of oxygen gave no more reliable endpoints.

The total amount of Cr(II) oxidized as measured by the current integrator was typically 4-10% less than the amount added to the cell. It was felt that this was probably due to air oxidation of the Cr(II). To check this the cell was filled as for an electrolysis and aliquots

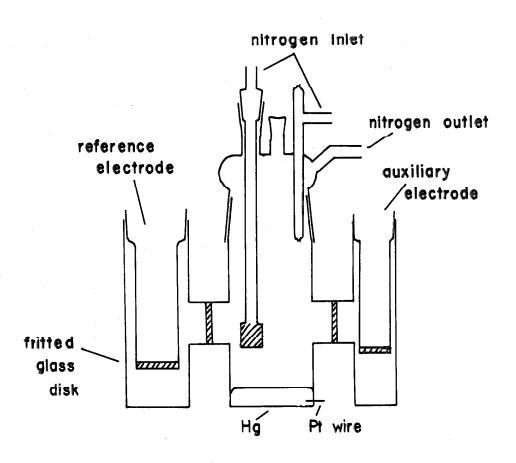


Figure 5. Cell used in controlled potential electrolysis of Cr(II) solutions.

of the solution were analyzed for Cr(II) at intervals of 1/2 to 1 hr. The rate of decay of the Cr(II) concentration was found to be between 1 and 2 x 10^{-3} meq./min. which accounts roughly for the observed discrepancy. The inclusion of chloride by Cr(II) on air oxidation is negligible (20).

Discussion. Proof that Cr(II) is electrochemically oxidized in the presence of chloride via a chloride bridge raises more specific questions about the mechanism. The inclusion of chloride by Cr(II) specifies the transition state but does not tell us how the transition state is formed. In order to understand the reaction we need to know if CrCl⁺ complex formation prior to the electron transfer step is important. We also need to know more about the relationship between the absorption of chloride and the formation of the transition state. These questions are discussed further in Chapter 4.

The prominent characteristics of chloride in this context are:

- a) chloride increases the rate of oxidation of Cr(II) at mercury electrodes (6);
- b) chloride is adsorbed on mercury at those potentials where Cr(II) is oxidized (8);
- c) chloride acts as a bridge for electron transfer in the homogeneous oxidation of Cr(II) (2);

and, as we have shown,

d) chloride acts as a bridge for electron transfer in the oxidation of Cr(II) at mercury electrodes.

All ligands having a-c in common with chloride might also have d in

common. This certainly must be true of at least bromide and iodide.

The effects of bromide and iodide on the electrochemical oxidation of Cr(II) are discussed in Chapter 5 and Chapter 6.

Chapter 4

CHRONOPOTENTIOMETRIC INVESTIGATION OF THE OXIDATION OF CHROMIUM(II) IN THE PRESENCE OF CHLORIDE

Chronopotentiometry was used to investigate the effect of chloride on the oxidation of Cr(II) at mercury electrodes in more detail. The technique of chronopotentiometry has been throughly discussed by Delahay (21).

There are three purposes for investigating the reaction by chronopotentiometry. The first is to see if CrCl^+ is the species which reacts at the electrode. The second is to see if there is reactant adsorption. The third purpose is to show that the formation of $\operatorname{CrCl}^{2^+}$ in the oxidation of $\operatorname{Cr}(II)$ is quantitative when microcoulombs of $\operatorname{Cr}(II)$ are oxidized as well as in mass electrolysis.

By observing the variation of the chronopotentiometric constant with current density one can determine the presence of a chemical reaction preceding the electron transfer step or detect the oxidation of material adsorbed on the electrode. In the former case the chronopotentiometric constant decreases with increasing current density. This occurs when the rate of electron transfer demanded by the controlled current becomes comparable to the rate of the prior chemical reaction. The upper limit for detection of rate constants is approximately $500 \ \sec^{-\frac{1}{2}} \text{ for the product } k_{\frac{1}{2}}(k_{\frac{1}{2}}+k_{\frac{1}{2}})^{\frac{1}{2}}/k_{\frac{1}{2}}$ where the rate constants apply to the reaction scheme

$$Y \xrightarrow{k_{f}} 0 \xrightarrow{+ne} R \tag{1}$$

The preceding reaction of interest to us is

$$\operatorname{Cr}^{2^{+}} + \operatorname{Cl}^{-} = \operatorname{Cr}\operatorname{Cl}^{+} \tag{2}$$

The complex formation constant for $CrCl^+$ is less than 5×10^{-4} l./mole (7) so the upper limit for detection of $(k_f + k_b)$ is about 10^{12} sec.⁻¹. This limit is high enough that absence of kinetic effects rules out Reaction 2 as an important step in the oxidation mechanism.

In the case of adsorption, the chronopotentiometric constant increases with increasing current density. In the absence of any complications this product should be constant. That means that the higher the current density the smaller the number of equivalents of diffusing material oxidized, as that is proportional to it, not it. If n $\Im\Gamma$ equivalents of adsorbed material are on the electrode, current must go to the oxidation of the adsorbed material, thus decreasing the current going to diffusing material and hence increasing the transition time. This effect can be seen when n $\Im\Gamma$ is as large as 10% of it for the diffusing material. Since chloride is adsorbed on the electrode, it is possible that the chloride bridged oxidation of Cr(TT) should show reactant adsorption.

A third and qualitatively different use of chronopotentiometry to study the reaction is the use of chronopotentiometry with current reversal to study the reaction product. For such a study to be possible the reduction of CrCl^{2^+} must occur at potentials anodic to Cr^{3^+} and the two waves must be clearly separable. If there is no adsorption of CrCl^{2^+} and if CrCl^{2^+} is formed quantitatively during the oxidation time,

the reverse wave for reduction of $CrCl^{2+}$ should be 1/3 as long as the forward time during which $CrCl^{2+}$ is formed. Failure to form $CrCl^{2+}$ quantitatively during the forward time should shorten the reverse time or increase the ratio of the forward to the reverse time.

Chronopotentiograms for Cr(II) in the presence and absence of chloride are shown in Figures 7 and 6, respectively. The current density for these waves is about 10 ma./cm.² It is necessary to use large current densities in order to obtain a distinct transition for the reverse wave. The large potential separation between the forward and reverse waves in Figure 6 indicates that the Cr(II)/Cr³⁺ couple is highly irreversible. The standard potential for the couple is -0.647 v. vs. SCE (22). The anodic and cathodic background reactions are $\text{Hg} \rightarrow \text{Hg}^{2+} + 2\text{e}^{-}$ and $\text{H}^{+} \rightarrow \frac{1}{2} \text{Hg} + \text{e}^{-}$, respectively.

In Figure 7 we see that the oxidation of Cr(II) occurs at a much more negative potential in the presence of chloride. On current reversal a wave for the reduction of CrCl²⁺ is obtained as expected. The couple Cr(II)/CrCl²⁺ is quasi-reversible. An indistinct wave for the reduction of Cr³⁺ precedes H⁺ reduction. The anodic background reaction in this case is calomel formation. The appearance of several waves is characteristic of mercury oxidation at high chloride concentrations with high current densities.

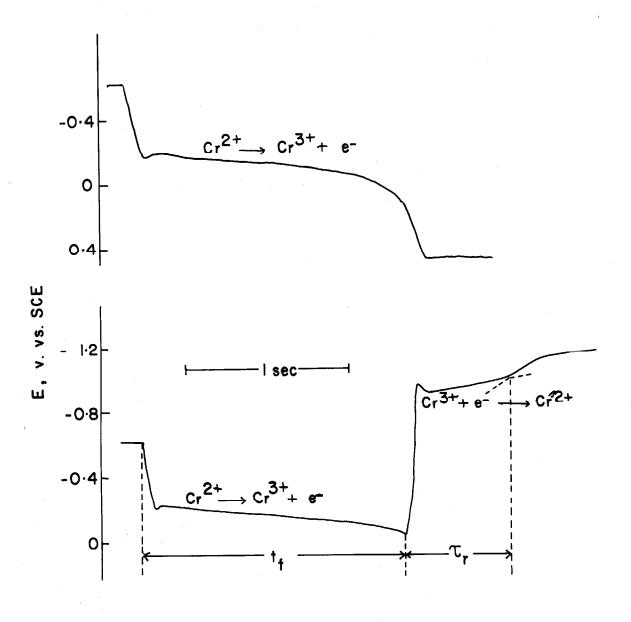


Figure 6. Chronopotentiometric behavior of Cr(II) in the absence of complexing ligands. Solution: 40 mF Cr(II) in 2 F HClO₄.

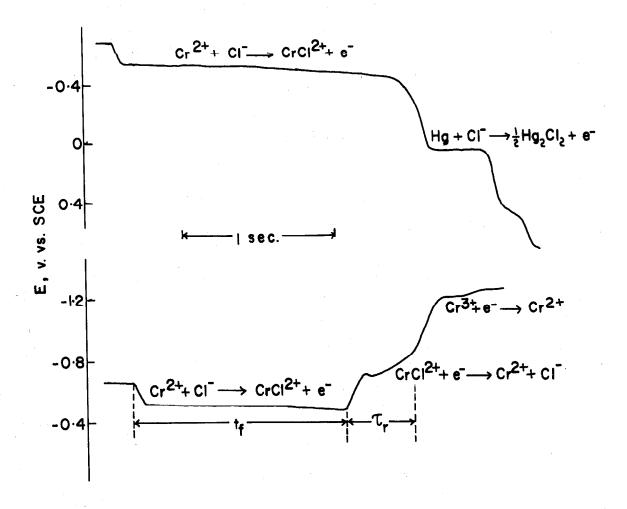


Figure 7. Chronopotentiometric behavior of Cr(II) in the presence of chloride. Solution: 40 mF Cr(II) in 0.5 F NaCl, 2 F HClO4.

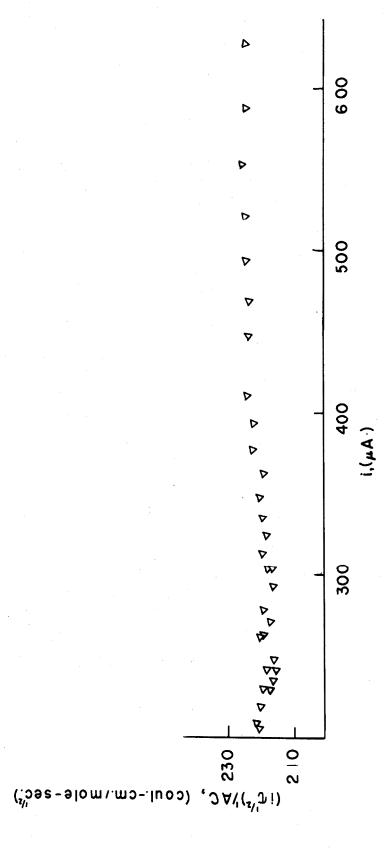
I. Chronopotentiometric Behavior of Cr(II) in the Absence of Chloride

1. <u>Variation of the Chronopotentiometric</u> Constant with Current Density.

The constancy of the chronopotentiometric constant with current density for Cr(II) in the absence of chloride is presented in Figure 8. Each τ value is an average of six trials. The values of $i\tau^{\frac{1}{2}}$ are corrected for spherical diffusion as described in Appendix I. The slight trend to lower values of the chronopotentiometric constant at low current densities is caused by departure from the conditions of spherical diffusion due to the volume excluded by the support for the hanging mercury drop electrode (Figure 13). This point is discussed further in Appendix I. The constancy of the chronopotentiometric constant with current density shows that the reaction is a simple electron transfer within the limits of the experimental conditions.

2. Reverse Current Chronopotentiometric Behavior.

The reverse current chronopotentiometric behavior of Cr(II) was studied in solutions 30 mF in Cr(II) and 2 F in HClO4. The current density was 4 ma./cm.² Two values of the ratio t_f/τ_r as defined in Figure 6 were obtained, each an average of five measurements. The values are 2.96 ± 0.09 and 3.03 ± 0.10 . The closeness of these values to the theoretical value of 3.00 is somewhat misleading, for the raw ratios should be corrected upward approximately 8% to subtract out the effect of ${\rm Cr}^{3^+}$ present in the solution, and corrected downward by approximately 8% to account for spherical diffusion effects for the 3-4



Constancy of the chronopotentiometric constant as a function of current for Cr(II) oxidation in the absence of complexing ligands. Solution: 37 mF Cr(II) in 2 F $HClO_4$. Electrode area 0.0566 cm.2 Figure 8.

sec. forward times (cf. Appendix I).

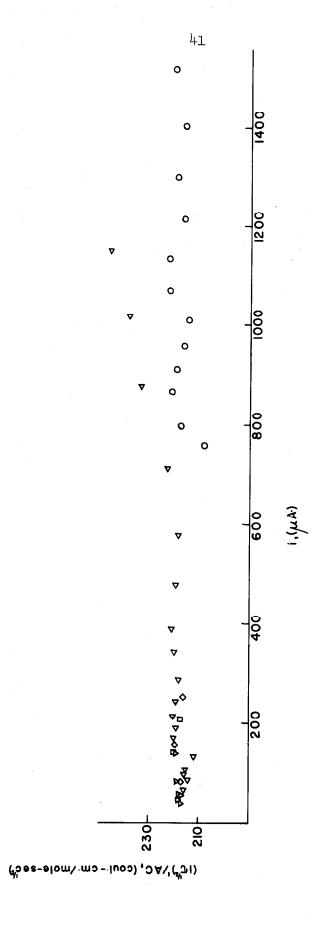
The correction for the finite bulk concentration of $\operatorname{Cr}^{\operatorname{st}}$ cannot be made directly by subtraction of a cathodic blank because that transition time was too short and indistinct to measure. Instead it was calculated from the decrease in the forward transition time for $\operatorname{Cr}(\operatorname{II})$ from the time when the solution was added to the cell.* The correction for spherical diffusion was calculated assuming no bulk concentration of the oxidized form. It should be emphasized that very small deviations from the true values of t_f and $\operatorname{\tau}_r$ can make a very large change in the value of the ratio. However, the agreement shown above is fairly convincing evidence that there are no unexpected effects in the oxidation and reduction of $\operatorname{Cr}(\operatorname{II})$ in the absence of complexing ligands.

II. Chronopotentiometric Behavior of Cr(II) in the Presence of Chloride

1. <u>Variation of the Chronopotentiometric</u> Constant with Current Density.

The chronopotentiometric behavior of Cr(II) in the presence of excess chloride was studied under a variety of conditions. The results are presented in Figure 9. There is clearly no variation of the chronopotentiometric constant with current density. These results show no complications for the oxidation of Cr(II) in the presence of chloride over the range of conditions employed.

^{*}A portion of the Cr(II) lost goes to Cr(III) dimers which are not reduced with Cr3+ (23).



Constancy of the chronopotentiometric constant as a function of current for Cr(II) oxidation in the presence of chloride. Solutions: 4 4.0 mF Cr(II) in 0.100 F NaCl; O 2.9 mF Cr(II) in 0.100 F NaCl;

9.4 mF Cr(II) in 79.4 mF NaCl;

V 4.25 mF Cr(II) in 0.100 F NaCl; \clubsuit 12.2 mF Cr(II) in 0.100 F NaCl. All solutions 0.100 F HClO_{\updownarrow} (μ = 1.00). Figure 9.

2. Reverse Current Chronopotentiometric Behavior.

The reverse current chronopotentiometric behavior of Cr(II) in the presence of chloride was studied in solutions 2 F in HClO₄, 0.5 F in NaCl, and 30 mF in Cr(II). Using forward times of 1-2 sec., values of 2.97 ± 0.07 and 3.15 ± 0.02 were obtained for the ratio of the forward time to the reverse transition time at currents of 263 and 225 μ a., respectively. Each ratio is an average of five values. These values are corrected for spherical diffusion, the correction varying from 5 to 9% over the range of forward times used.

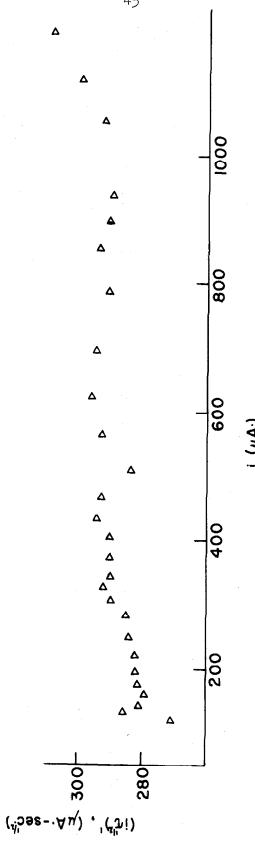
These results are adequate proof that in strong chloride solutions Cr(II) is quantitatively oxidized to CrCl²⁺ as is to be expected from the results of the controlled potential experiments.

3. The Chronopotentiometric Behavior of CrCl2+.

The chronopotentiometric behavior of the product complex, $\operatorname{CrCl}^{2^+}$, was investigated in order to confirm the conclusions drawn above. It is possible that the theoretical value of 3.00 for the ratio of forward time to reverse transition time for the oxidation of $\operatorname{Cr}(II)$ in chloride solution can be achieved by the cancellation of two competing factors. The first, which tends to increase the ratio, is failure to form $\operatorname{CrCl}^{2^+}$ quantitatively during the anodic process. The second, which tends to decrease the ratio, is adsorption of the product, $\operatorname{CrCl}^{2^+}$. The latter possibility can be rendered extremely implausible by verifying that $\operatorname{CrCl}^{2^+}$ is not adsorbed from solution.

The constancy of the chronopotentiometric constant with current density for ${\rm CrCl}^{2^+}$ reduction is illustrated in Figure 10. The trend toward lower values of the chronopotentiometric constant at low current





. Solution: 20 mF 3rCl3 Constancy of $(i\pi^2)^1$ with current for the reduction of $(rCl^{2^+})^1$ in 0.100 F HClO₄ (μ = 1.00). Figure 10.

densities is discussed above (page 38). The trend to higher values at high current densities is thought to be an experimental artifact (cf. Figure 9). These results show that the reduction of CrCl²⁺ is not complicated by prior reaction or adsorption.

The reverse current chronopotentiometric behavior was also studied. The following values of $t_{\rm f}/\tau_{\rm r}$ were obtained:

<u>i(μa.)</u>	$\frac{t_f/\tau_r}{}$
180	3.04 ± 0.01
142	3.03 <u>+</u> 0.05
42	3.07 ± 0.04
4.2	3.72 ± 0.12

It is suspected that the high value for the ratio obtained at low current densities is attributable to the method of transition time measurement which tends to give low values for the transition times of indistinct waves such as those obtained for Cr(II) at low current densities. These results show that there is no product adsorption.

III. Experimental Details

Equipment. Chronopotentiometric experiments were carried out using the circuit shown in Figure 11. The time delay circuit was suggested by Mr. George Lauer of CIT. This circuit is designed to allow pre-potentiostated chronopotentiometry with automatic current reversal at short times. It differs from more typically used and more satisfactory circuits in that the working (indicator) electrode is not grounded. This was not possible here because of severe pick-up of 30 Mc. noise if

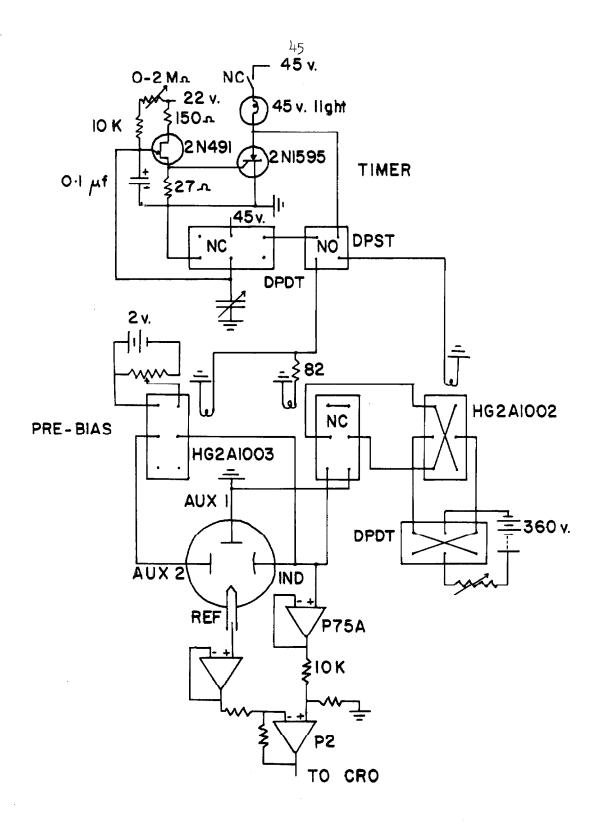


Figure 11. Circuit used in chronopotentiometric experiments.

the working electrode was grounded. All high frequency pick-up was eliminated by grounding the auxiliary electrode. This circuit is not recommended for general use.

In most experiments it was necessary to adjust the initial potential of the auxiliary electrode to that of the indicator electrode to avoid a current pulse when these two electrodes were shorted by the DPDT make-before-break relay which initiates the current flow through the cell.

Chronopotentiograms were recorded using either a Moseley X-Y
Autograf recorder or a Tektronix Type 531 oscilloscope with Type D Plugin Unit, depending on the time scale of the experiment.

The cell used in most of the chronopotentiometric experiments is pictured in Figure 12. Figure 13 shows some of the accessories. The volume of solution held by the center compartment is approximately 270 ml. This large volume was chosen so that the total amount of Cr(II) in the cell would be fairly large, since the rate of loss of Cr(II) seems to be independent of the concentration or amount of Cr(II) present.

The cell was surrounded by a water jacket (not shown) through which constant temperature water was circulated to maintain the temperature at 27.0° C.

A separate auxiliary compartment was used because Pt catalyzes the reduction of water by Cr(II).

The indicator electrode, 7 in Figure 8, is a hanging mercury drop electrode of the Shain type. Drops of mercury are collected from the DME (5) in the spoon (6) and transferred to the amalgamated platinum button (7). The platinum button was made by sealing 0.020 in. platinum

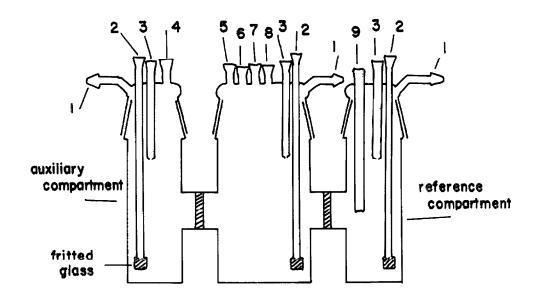


Figure 12. Cell used in chronopotentiometric experiments. 1: gas outlet to trap; 2,3: N2 inlets; 4-7: inserts (see Figure 13); 8: delivery tube from Cr(II) reservoir; 9: salt bridge of L&N SCE reference electrode.

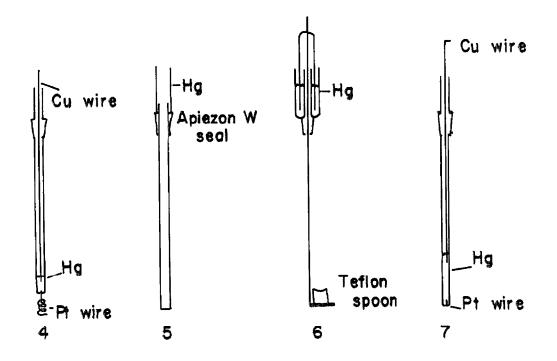


Figure 13. Cell inserts. See Figure 12. 4: auxiliary electrode; 5: dropping mercury electrode; 6: teflon spoon with mercury seal; 7: indicator electrode.

wire in pyrex, and then grinding the end flat. The button was amalgamated by dipping it into sodium amalgam and washing with water.

The sodium amalgam was prepared by dissolving sodium in mercury.

Three drops from the DME were used for the hanging drop electrode. The radius was 0.0671 cm. and the area 0.0566 cm.² as calculated from the weight of 50 drops.

The reference electrode was an L&N SCE whose salt bridge was sealed directly into the cell. The salt bridge was filled with saturated NaCl solution before each experiment. The electrode itself was soaked in saturated NaCl solution between experiments. This treatment prevented any KClO₄ precipitation during experiments even though the electrode itself still had KCl present. The potential of the electrode remained within the 12 mv. range between the KCl-SCE and NaCl-SCE. This partial conversion of a commercial SCE to NaCl-SCE is more difficult with electrodes having one piece construction.

The outlet trap consists of successive flasks containing V(II) in 1 F H_2SO_4 and water, respectively. The V(II) solution was kept in the reduced state by zinc amalgam.

Materials. The nitrogen used was CIT nitrogen purified by passing through successive gas washing towers containing 0.1 F V(II) in 1 F H₂SO₄, 0.1 F Cr(II) in 1 F H₂SO₄, and water. The V(II) and Cr(II) solutions were kept over zinc amalgam.

Cr(II) stock solutions were prepared by electrolysis as described in Chapter 2.

Sodium chloride was purified by precipitation from NaCl solution with HCl gas liberated from 12 F HCl by slowly adding 18 F H₂SO₄.

Sodium perchlorate stock solutions were prepared by filtering freshly prepared saturated NaOH solution into a known quantity of analyzed concentrated HClO₄ (60%) until the resulting solution was neutral to pH paper and then diluting to volume. Iron, which occurs as a significant impurity in NaOH, is quantitatively precipitated as Fe(OH)₃ on standing for several weeks. The solution, after filtering, is then ready for use.

This method of preparing NaClO₄ solutions is preferred over the addition of $HClO_4$ to Na_2CO_3 because of the extreme persistence of carbonate in non-equilibrium concentrations. $NaClO_4$ solutions made with Na_2CO_3 on standing slowly develop a white gelatinous precipitate, probably $Mg(OH)_2$.

The source of $\operatorname{CrCl}^{2^+}$ was Baker and Adamson Chromium Chloride which has the formula $\operatorname{CrCl}_2(H_2O)_4 \cdot \operatorname{Cl}$. The major cationic species of this salt is CrCl_2^+ which rapidly dissociates in water to give $\operatorname{CrCl}^{2^+}$. Solutions were prepared by adding a small amount of the salt to a convenient volume of supporting electrolyte solution 0.1 F in HClO_4 and 0.9 F in NaClO_4 or 0.1 F in HClO_4 and 0.9 F in NaClO_4 or 0.1 F in HClO_4 and 0.9 F in NaClO_4 . The concentration of the resulting solutions was 5-20 mF in $\operatorname{CrCl}^{2^+}$.

Procedures. Experiments were carried out in the following manner. A measured volume of supporting electrolyte solution with the desired concentrations of NaCl, HClO₄, and NaClO₄ was added to the cell and the solution and cell purged of oxygen. The dropping mercury elec-

trode and Cr(II) reservoir were then put in place and after further deacration and subsequent examination of the chronopotentiometric behavior of the background solution, the desired amount of Cr(II) stock solution was added through the delivery tube. The solutions are specified by their formal concentrations of Cr(II), HClO₄, NaCl, and the ionic strength. It is understood that NaClO₄ is present as required to give the specified ionic strength.

Treatment of data. Transition times were measured by the method of Voorhies and Furman (24). Correction for the current going to double layer charging was made where indicated by the initial slope of the chronopotentiometric wave.

Transition times are corrected for spherical diffusion as described in Appendix I. Corrected values of the product $i^{\frac{1}{2}}$ are designated $(i^{\frac{1}{2}})^{!}$.

Experiments designed to determine the constancy of $i\tau^{\frac{1}{2}}$ with change in current density are complicated by the gradual decrease in the Cr(II) content of the solution due to air oxidation. Typically the Cr(II) concentration changed at a rate corresponding to 0.05 to 0.2 millimoles/hour. For this reason it was desirable to work at Cr(II) concentrations as high as possible. This has the second advantage of requiring much higher current densities which in turn sharpens the poorly defined Cr(III) reduction wave.

In order to take into account the decrease in Cr(II) concentration during the course of an experiment, the Cr(II) concentration was measured chronopotentiometrically at a fixed current density at intervals of 20 minutes during each run. The concentrations of Cr(II) were plotted versus real time to obtain the instantaneous bulk concentration of Cr(II). The chronopotentiometric constant presented is calculated using this instantaneous concentration. The measured values of the concentration did not always lie on a smooth curve but the concentration was obtained as a function of real time by the best smooth curve through the points. This simply increases the scatter of the points and does not affect the general reliability of the results.

IV. Discussion

The smallest it product is about 1 μ C and the shortest transition time about 1 ms. for these experiments. These two values fix the maximum amount of reactant adsorption and the minimum value of the product $k_f(k_f + k_b)^{\frac{1}{2}}/k_b$ for a prior chemical reaction. Assuming that a 10% variation in the chronopotentiometric constant indicates adsorption or prior chemical reaction, these limits are 1 μ C/cm.² of adsorbed material and $k_f(k_f + k_b)^{\frac{1}{2}}/k_b = 500$ sec. $\frac{1}{2}$, respectively. These limits are extreme enough to imply that neither Cr(II) oxidation nor CrCl²⁺ reduction is complicated by reactant adsorption or prior chemical reaction.

The absence of any evidence for reactant adsorption in either case shows that the reaction does not proceed via a long lived adsorbed intermediate. Absence of kinetic complications shows that CrCl⁺ formation is not important to the chloride bridge oxidation mechanism.

These results eliminate two processes which were potentially important in bridge formation. However, the role of adsorbed chloride is still not well-defined. We can obtain more specific information

about the role of adsorbed halide by studying the effects of bromide and iodide on Cr(II) oxidation at mercury electrodes. Either ligand might have some unexpected effect that would clarify the role of adsorption. Failing this, a comparison of the effects of the three ligands should give some mechanistic information.

Chapter 5

THE OXIDATION OF CR(II) AT MERCURY ELECTRODES IN BROMIDE SOLUTIONS

The smooth gradation in most of the properties of the halides from chloride through iodide leads us to predict that the effect of bromide on the oxidation of Cr(II) will be qualitatively similar to that of chloride.

Typical reverse current chronopotentiometric behavior of Cr(II) solutions with large excess bromide is shown in Figure 14. The reverse wave is for the reduction of CrBr²⁺. The apparent reversibility is much greater than in the case of chloride (Figure 7). It is also interesting to note that the reduction of CrBr²⁺ takes place at potentials well anodic of the standard potential for the couple Cr(II)/Cr³⁺, -0.65 v. vs. SCE. This phenomenon is possible because the favored oxidation mechanism (ligand bridging) gives a thermodynamically unfavored product (CrBr²⁺) which is not in equilibrium with the thermodynamically favored product (Cr³⁺). It is, in fact, observed because the reduction of CrBr²⁺ is sufficiently reversible that the chronopotentiometric wave occurs near the half-wave potential for the couple Cr(II)/CrBr²⁺. This is in contrast with Cr³⁺ which is so irreversibly reduced that under most circumstances there is concomitant hydrogen ion reduction.

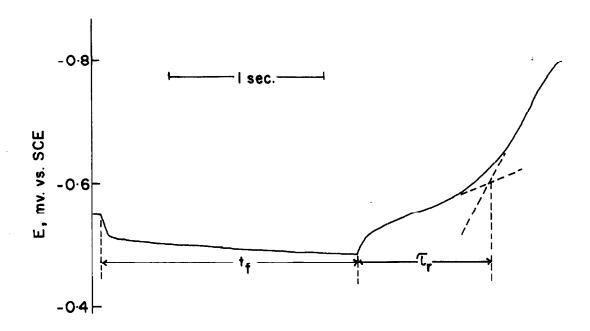


Figure 14. Chronopotentiometric wave with current reversal for Cr(II) in bromide solution. Solution: 2.65 mF Cr(II) in 0.100 F NaBr, 0.100 F HClO₄ (μ = 1.00). i_0 = 155 μ A./cm.²

I. Chronopotentiometric Behavior

1. Variation of the Chronopotentiometric Constant with Current Density; Solutions Containing Excess Bromide.

The oxidation of Cr(II) in excess bromide was studied chronopotentiometrically. It was found that there is no variation of the chronopotentiometric constant with current density as is illustrated in Figure 15. This shows that the reaction is a simple electron transfer as described in Chapter 4.

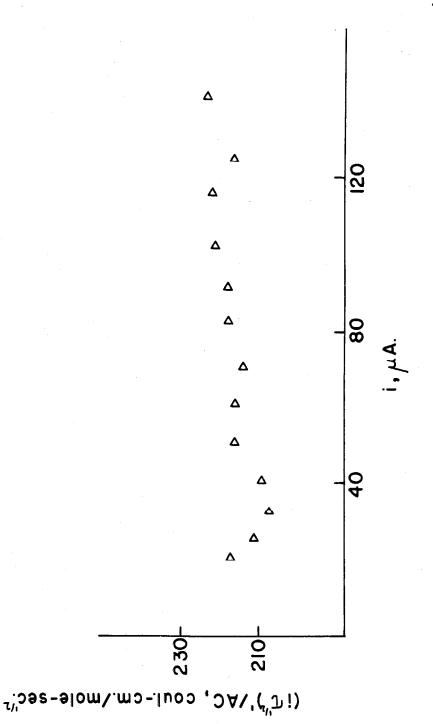
Experimental procedures. The equipment and procedures used in the investigation of the constancy of the chronopotentiometric constant with current density are described in Chapter 4.

Sodium bromide was purified by treating a hot saturated solution of the salt with decolorizing charcoal, recovering the salt as NaBr·2H₂O, drying at 150° C. to obtain the anhydrous salt, and recrystallizing it twice from absolute cthanol. This is an extremely unsatisfactory procedure and is not recommended.

2. Dependence of the Oxidation of Cr(II) on Bromide Concentration.

The oxidation of Cr(II) was also studied chronopotentiometrically in a series of solutions in which the concentration of Cr(II) was fixed and the bromide concentration varied from zero to an excess amount. The results are shown in Figure 16.* I shows the wave which appears for Cr(II) oxidation in the absence of bromide. The composition of the

^{*}The waves for Cr(II) exidation become slightly shorter from I to IV in Figure 16 due to air exidation of Cr(II).



Constancy of the chronopotentiometric constant as a function of current for Cr(II) oxidation in the presence of bromide. Solution: 2.65 mF Cr(II) in 0.100 F NaBr, 0.100 F HClO4 (μ = 1.00). Figure 15.

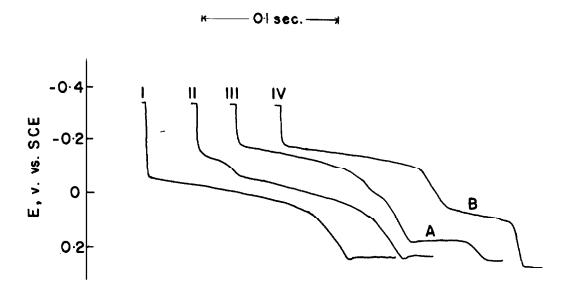


Figure 16. Chronopotenticmetric behavior of Cr(II) in solutions containing small amounts of bromide. Values of the flux ratio, (Br)DBr /2/(Cr(II)DCr are: I, 0; II, 0.39; III, 0.90; IV, 1.31.

solution is 0.219 F HClO₄, 15.1 mF Cr(II), 5.6 mF Cr³⁺ (μ = 1.00).

In II we see the result of adding sufficient sodium bromide solution to make the bromide concentration 3.04 mF. A new wave whose length corresponds to a bromide concentration of 3.10 ± 0.04 mF appears at a potential cathodic to the original Cr(II) oxidation wave. This wave is due to the oxidation of Cr(II) via a bromide bridge to form $CrBr^{2+}$.

Similar experiments were done in chloride solutions but there was no transition corresponding to a process diffusion limited by chloride. The fact that a transition appears in bromide solution indicates that the formation of $\operatorname{CrBr}^{2^+}$ via ligand bridging is more facilitated than the similar reaction with $\operatorname{CrCl}^{2^+}$ as its product. It should also be pointed out that the wave appearing in II is very sensitive to the experimental conditions. The absolute concentrations of $\operatorname{Cr}(\operatorname{II})$ and bromide as well as the current density must be properly adjusted in order to see the wave.

III shows the result of adding an almost equivalent amount of bromide. The transition time for the bromide dependent process cannot be measured because of the indistinctness of the wave, but there is clearly a transition limited by bromide diffusion before the much sharper break in potential associated with the Cr(II) concentration. The following wave (A) which occurs at approximately +0.135 v. is undoubtedly due to bromide. The question that immediately arises is why, if the concentration of bromide at the surface of the electrode is zero, as is required by the transition for the bromide diffusion limited process, does one see a wave which implies the presence of bromide. This is a

well documented and reproducible effect which occurs with other ligands as well as bromide (25).

The apparent contradiction between the absence of bromide and the presence of a mercurous bromide wave arises because attention is too closely focused on the condition that the concentration of bromide at the electrode surface is zero after the transition for the bromide diffusion controlled process. The important point is not this fact, but rather its cause, namely that the reaction rate demanded by the controlled current is greater than the rate of diffusion of bromide to the electrode. The initial potential break occurs because the rate of bromide diffusion is not sufficient to support the current demanded. A potential transition occurs then to a more anodic potential at which point a new reaction occurs, in this case the direct oxidation of Cr(II) unassisted by bromide. While on the plateau for the bromide-independent process, the oxidation of Cr(II) assisted by bromide continues at a rate determined by the rate of diffusion of bromide to the electrode. When the concentration of Cr(II) at the electrode surface is reduced to zero another transition occurs. At this point the potential shifts to a still more anodic value until a third reaction begins (A). By comparing II and III of Figure 16 we conclude that this reaction is due to bromide.

There is extensive evidence that there is more than one electron per bromide in the oxidation of mercury in the presence of bromide. This is illustrated in Figure 17 by the comparison of calculated and measured chronopotentiometric constants. It is also observed that in reverse current chronopotentiometry the first wave for mercury oxidation in the presence of bromide exhibits a reverse wave which is much shorter than

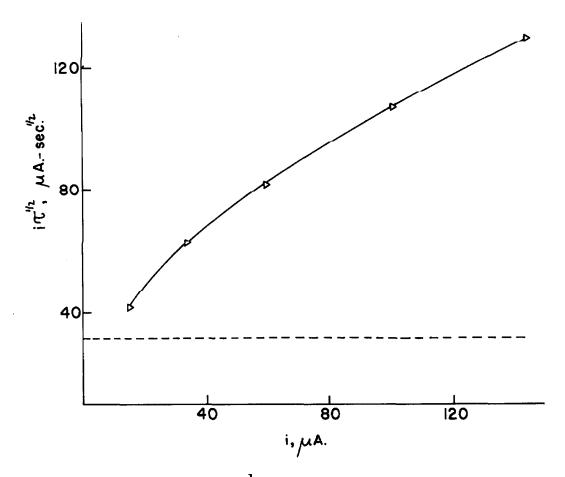


Figure 17. Variation of $i\tau^{\frac{1}{2}}$ with current for the oxidation of mercury in bromide solution. Solution: 1.01 mF NaBr, 0.088 F HClO₄ (μ = 0.99).

the forward time. This shows that the product of the oxidation is not simply Hg2Br2, for if that were the case the product would stay on the electrode and the forward and reverse times would be equal.

By analogy with work that has been done on calomel formation (26) we may reasonably assume that the initial product in mercury oxidation in the presence of bromide is HgBr^+ so that the effective value of a for bromide is 2. The rate of mercury oxidation is known to be rapid (27); it is probable that at the potential of the first mercury wave the rate for mercury oxidation to HgBr^+ and $\operatorname{Cr}(\operatorname{II})$ oxidation to $\operatorname{CrBr}^{2^+}$ are comparable and the two processes compete for bromide.

The effective n value of 2 for the mercury process momentarily increases the effect of bromide sufficiently to satisfy the current requirement. Assuming that the amount of current going to the mercury process is 1/3 of the total current, the bromide wave corresponds to $240~\mu\text{C/cm.}^2$ of material, which is a reasonable value for monolayer coverage. The sharp transition characteristic of processes which change the nature of the electrode surface is then due to the passivation which occurs when a monolayer of material has been deposited on the electrode.

These are plausible explanations for the observed behavior which are not intended to be conclusive. The possibility of devising experiments to clarify the observed behavior is limited by the complexity of the oxidation of mercury in the presence of bromide alone, which is as yet poorly understood.

In IV of Figure 16 we see a well developed wave for the oxidation of Cr(II) to $CrBr^{2+}$ in a significant excess of bromide over Cr(II). The Cr(II) wave is followed by a wave for mercury oxidation (B). The

potential of the wave B corresponds to that for Hg₂Br₂ formation at the calculated effective concentration of bromide. Its length does not correspond to that concentration; this is typically observed for oxidation of mercury in the presence of bromide. However, waves A and B are equal in length within the uncertainty in determining the transition time.

<u>Discussion</u>. A point arises in the preceding discussion of the bromide wave which, although not subtle, is sufficiently important to deserve further emphasis.

There is no mathematical distinction between saying that the concentration of bromide at the electrode surface is zero and saying that bromide is used up as fast as it arrives at the surface. The statement that the transition occurs when the concentration of the reacting material at the electrode surface has reached zero, and that the concentration remains zero from that time on is a general statement of general validity which applies as fully in this particular case as in more ordinary cases. The difficulty in interpretation arises because attention becomes focused on the simple statement of the boundary condition for the chronopotentiometric diffusion problem,

$$C(0,t \ge \tau) = 0 \tag{1}$$

and the physical situation giving rise to this condition is lost. The important thing to keep in mind is that for $t \ge \tau$ the effective rate for the removal of the reacting species at the electrode is greater than the rate of diffusion of that species to the electrode. This effective rate may be the sum of pseudo-first-order rates for several processes.

Experimental procedures. The circuitry, method of measurement, and solutions have been discussed above. The cell employed in these experiments is shown in Figure 18. The 0-ring joint provides a good solution to the problem of making a greaseless airtight seal between cell top and bottom. The cell volume is approximately 150 ml.

The reference electrode was a small Beckman SCE. The salt bridge was the cracked glass type made by sealing a soft glass bead into a pyrex tube. 1 F NaNO3 solution was used in the salt bridge.

The indicator electrode was a Kemula type hanging mercury drop electrode available from Brinkman Instruments, Inc. The electrode area was 0.0409 cm.² as calculated from the weight of 10 drops.

Mallinkrodt triple distilled quality mercury was used.

In these experiments the supporting electrolyte solution was added to the cell and the system deaerated. Then mercury was added to fill the two wells in the bottom of the cell (which served as mercury pool auxiliary electrodes) and the Kemula hanging mercury drop electrode was put in place. The seal between the Kemula electrode and the cell joint was made air tight with Teflon tape. Finally, after further deaeration the Cr(II) reservoir was put in place and the appropriate amount of Cr(II) stock solution added to the cell.

Successive 0.1 ml. portions of deaerated NaBr solution were added to the cell by syringe through a serum cap.

The same procedure was followed in other experiments using this cell with the exception that in most experiments it was not necessary to add solution to the cell after the Cr(II) had been added.

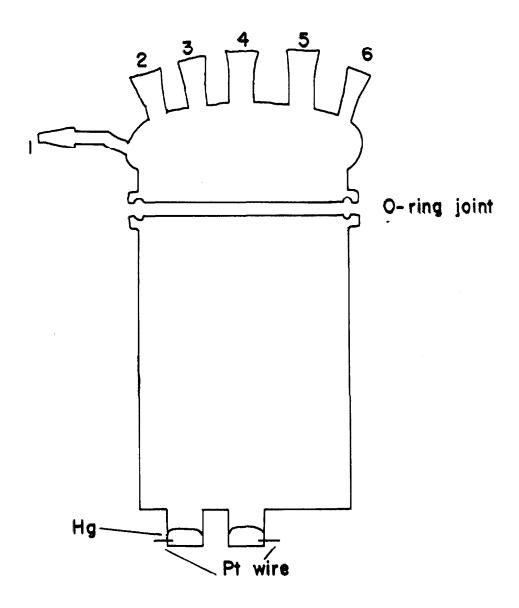


Figure 18. Cell used for electrochemical studies on Cr(II) solutions.
1: to outlet trap; 2: N2 inlet; 3: salt bridge for reference electrode; 4: Kemula indicator electrode; 5: spare; 6: Cr(II) inlet.

The cell shown in Figure 18 was also provided with a water jacket (not shown) which in conjunction with a constant temperature bath was used to maintain the temperature at 27.0° C.

3. Reverse Current Chronopotentiometric Behavior;

Large Excess Bromide.

The oxidation of Cr(II) in excess bromide was investigated using reverse current chronopotentiometry in order to determine if the product of the oxidation is entirely CrBr^{2^+} . If complete inclusion does occur, and the results are appropriately corrected for the effects of spherical diffusion as discussed in Appendix I, the ratio of the forward time, t_f , to the reverse time, τ_r , as defined in Figure 14 should be 3.00.

Figure 19 gives some results obtained in 0.1 F bromide solution with 2.65 mF Cr(II). The dotted line shows the expected ideal behavior. Each point is an average of 3 to 7 measurements. The forward times are in the range 1.4 to 2.1 sec. and the currents 4 to 24 μa . The values are not corrected for spherical diffusion. However, as shown in Appendix I, the effect of spherical diffusion is to increase the value of the ratio t_p/τ_r , which would shift the points below the dotted line.

Several possible explanations for this behavior can be ruled out. The current was measured during the forward and reverse waves and found to be constant to 0.2%. There was no anodic current spike on reversal. The cathodic background was carefully checked. No trace of reducible impurities was found. Product adsorption during the anodic cycle is virtually ruled out by the ideal behavior of CrBr²⁺ reduction, which is demonstrated below.

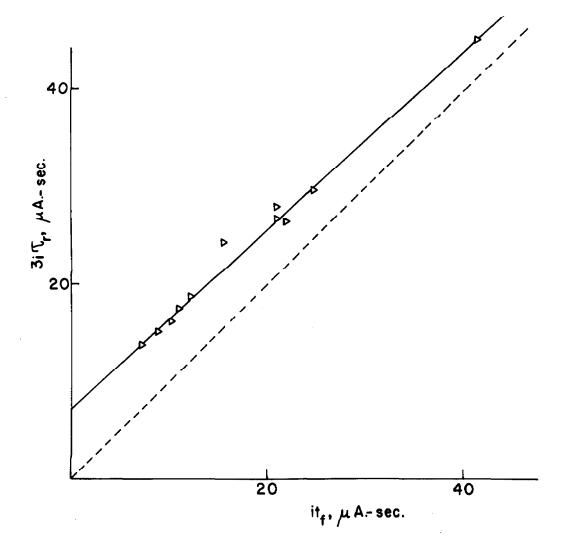


Figure 19. Reverse current chronopotentiometric behavior of Cr(II) in bromide solution. Solution: 2.65 mF Cr(II) in 0.100 F NaBr, 0.100 F HClO₄ (μ = 1.00). The dotted line shows the expected behavior for an ideal system under conditions of linear diffusion.

It is suggested that the abnormally long reverse waves are due to having oxidized material trapped in the wedge-shaped volume above the drop and below the glass capillary. This trapping effect is discussed in more detail in Appendix I.

For purposes of comparison some data for the reverse current behavior of an ideal system, Fe(II) in pyrophosphate solution at pH 2, is presented in Figure 20. These data were obtained at a current of 15 μ a. with t_f in the range 1.5 to 3.0 sec. The behavior is seen to be the same as that for Cr(II) oxidation in bromide solution.

Experimental procedures. The chronopotentiometric circuit is shown in Figure 11 and the cell in Figure 18.

Other experimental details are discussed on Page 64.

The experiments on the Fe(II) system are discussed in more detail in Appendix I.

<u>Discussion</u>. These results are marred by the failure of the experimental conditions to correspond to the simple spherical diffusion case. However the explanation for the deviation of the results from the expected behavior is sufficiently convincing that these results are considered to be an adequate demonstration that in solutions with large bromide concentration the product of the oxidation of Cr(II) is entirely CrBr²⁺.

4. Solutions with Low Bromide Concentration

The results presented thus far for the oxidation of Cr(II) in the presence of bromide show the behavior predicted by the ligand bridging

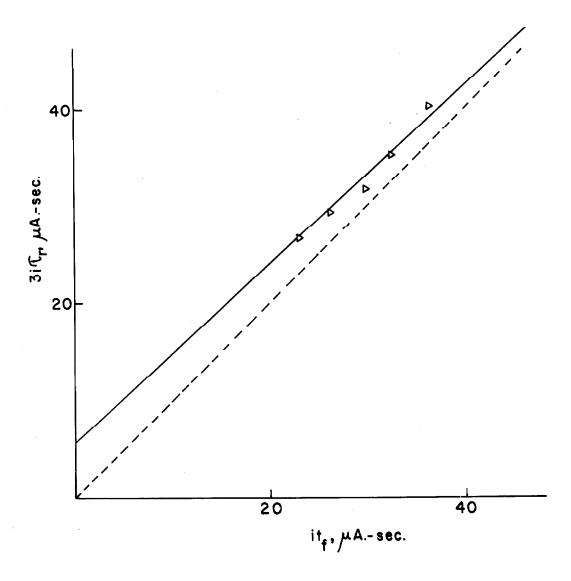


Figure 20. Reverse current chronopotentiometric behavior for an ideal system, Fe(II) in pyrophosphate. Solution: 30 mF FeSO₄ in 0.5 F Na₄P₂O₇, pH 2. The dotted line shows the expected behavior for conditions of linear diffusion.

model. The situation is somewhat more complex in solutions with very low bromide concentration.

The reverse current chronopotentiometry of Cr(II) was studied in solutions with 1.00 mF NaBr, 1.80 mF Cr(II), 0.100 F $HClo_4$ (μ = 1.00). These concentrations provide equal fluxes of Cr(II) and bromide. Over a wide range of conditions the ratio of forward to reverse times was found to be in the range 5.00 to 5.75. This shows a pronounced shortening of the reverse wave and is clear evidence for lack of complete inclusion of bromide under conditions where there is at least a stoichiometrically equivalent amount present at the electrode.

Similar experiments were done in solutions with 20 mF Cr(II). In this case the forward time was restricted to values less than the calculated transition time for bromide at the current density used. This insured that there was always a stoichiometric excess of bromide at the electrode. The reverse wave obtained was always much shorter than 1/3 of the forward time.

It was found that the ratio of forward to reverse times is potential dependent under these conditions. As an illustration, some results obtained with a current of about 10 μa . and a forward time of approximately 3 sec. are presented in Table 4.

TABLE 4

E, mv. vs. SCE	$\frac{t_f/\tau_r}{}$
-440	106
-420	31.2
-1400	13.6
-380	9.58
-37 ^C	7.50
-360	6.45

For the current density used, the potential was constant to within 10 mv. for at least the final 2/3rds of the forward time. This value is given to the nearest 10 mv. in Table 4. The variation in potential is difficult to explain in detail but is not surprising because the amount of CrBr²⁺ formed depends on but also determines the potential.

From those results it is clear that the fraction of $CrBr^{2+}$ in the product of Cr(II) oxidation is a strong function of the potential at which the oxidation occurs, and that the more anodic that potential, the larger the percent of bromide inclusion. This in turn suggests that the technique of chronopotentiometry is ill suited to the study of the problem, for potential dependence of the results implies that only a method which employs potential control will yield any definitive information or more detailed information about the mechanism.

The behavior in 3.6 mF Cr(II) was found to be that to be expected in view of the above discussion. Reverse current chronopotentiometry showed a variation of forward time to reverse transition time ratios from 4 to 10. The ratio depended heavily on current density as one

would expect, for at higher current densities, the wave, being irreversible, is shifted to more anodic potentials, and a higher fraction of bromide inclusion occurs.

5. Summary and Discussion.

The chronopotentiometric experiments in Cr(II) solutions with bromide present demonstrate the following points.

- 1) At sufficiently large bromide concentrations the product of oxidation of Cr(II) in the presence of bromide is entirely CrBr^{z+}.
- 2) The oxidation does not always result entirely in the product $\operatorname{CrBr}^{2^+}$ when there is a stoichiometric excess of bromide.
- 5) The fraction of the product appearing as CrBr²⁺ when a mixture of CrBr²⁺ and Cr³⁺ is formed is potential dependent and is greater at more anodic potentials.

These results provide a qualitative description of the processes going on at the electrode and agree well with results obtained in chloride solutions. A quantitative discussion of the behavior is not possible from the chronopotentiometric results because chronopotentiometry is inherently unable to give detailed information about potential dependent processes. To obtain that information it is necessary to turn to experimental methods which employ potential control rather than current control. A more detailed discussion of the implications of the chronopotentiometric results is inappropriate without consideration of the results presented below.

II. Double Potential Step Chronocoulometric Behavior

The principles of double potential step chronocoulometry are developed and discussed in detail by Christie et al. (28,29). The application of this technique to the study of the oxidation of Cr(II) in bromide solution is fruitful because, as suggested by comparison of Figure 6 and Figure 14, CrBr²⁺ is reduced at sufficiently anodic potentials that potentials exist for which the reduction of CrBr²⁺ is diffusion limited but no reduction of Cr³⁺ occurs. The application of the technique is illustrated in Figure 21 which shows the potential function applied to the cell and the resulting charge/time behavior for the faradaic reaction.

In order to use this method with confidence it is first necessary to define the range of potential for which CrBr2+ is reduced and verify that that reduction is ideally behaved.

1. The Reduction of CrBr2+.

The ideal behavior of the reduction of $CrBr^{2^+}$ under potential step chronocoulometric conditions is illustrated in Figure 22. The agreement of intercepts with measured intercepts for double layer charging and the constancy of slope was maintained for starting potentials in the range -0.200 to -0.300 v. vs. SCE and final potentials in the range -0.750 to -0.850 v. vs. SCE. The definition of allowable final potential is of importance, for the potential must be sufficiently cathodic that the electrode reaction is diffusion controlled, yet sufficiently anodic that no Cr^{3^+} present is reduced.

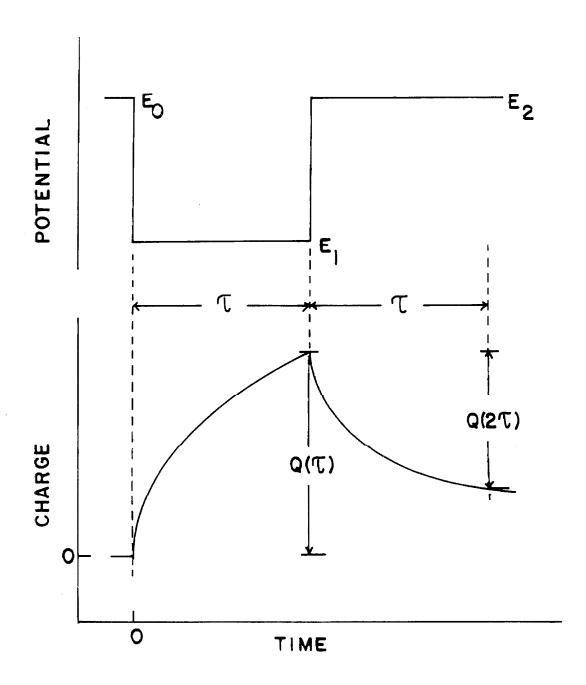
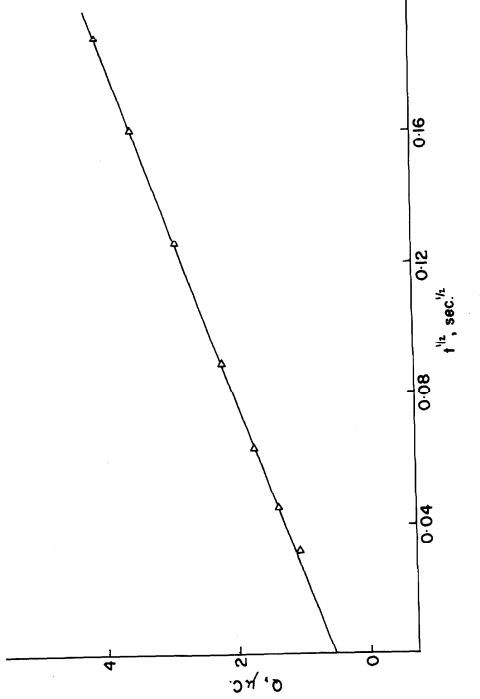


Figure 21. Typical double potential step chronocoulometric behavior.



Potential step behavior for CrBr²⁺ reduction. Solution: 1.7 mF CrBr³ in 0.100 F HClO₄ (μ = 1.00). The measured double₁ layer charging blank is 0.52 μ C. The slope of the line, 18.9 μ C./sec.², corresponds to a Cr(II) concentration of 1.67 mF. Figure 22.

The agreement of intercepts also indicates that CrBr2+ is not adsorbed in significant amounts.

Experimental details. These experiments were carried out with the aid of a general purpose electrochemical instrument using solid state amplifier circuitry. The instrument was designed by Mr. George Lauer of C.I.T. and is described in detail in his thesis (30).

The indicator electrode was a Kemula hanging mercury drop electrode available from Brinkman Instruments, Inc. It was used in conjunction with a cell of standard design, also from Brinkman.

The reference electrode was a small Beckman SCE. The auxiliary electrode was a piece of platinum wire.

Solutions were purged of oxygen with a stream of prepurified nitrogen. Flow of nitrogen through the cell above the solution was maintained during the course of each experiment.

Supporting electrolyte solutions were 0.1 F $HClO_4$ with NaBr variable and NaClO₄ to maintain μ = 1.00. Free bromide concentration in the solutions investigated varied from approximately 0.5 F to 3 mF.

The source of CrBr²⁺ was Chromic Bromide available from K&K Laboratories, Plainview, New York. The major cation of this salt is CrBr₂⁺ which rapidly dissociates in water to give the complex CrBr²⁺. This complex is sufficiently stable (see Chapter 2) that no correction for dissociation of the salt need be made for times less than about 30 min.

The experiments were carried out in the following manner. The amount of charge required to charge the double layer when the potential

is stepped from the initial to the final potential was measured in the deaerated supporting electrolyte solution for the potentials of interest. A small amount of the dry Chromic Bromide salt was then added to the cell and the solution deaerated further for about five minutes to allow for complete decomposition of the dibromo complex.

Q - t curves obtained from the potential steps were displayed on a Tektronix Type 564 storage oscilloscope equipped with Type 3A72 and 3B3 Plug-In units. Satisfactory traces were recorded on Polaroid film.

2. The Inclusion of Bromide in Cr(II) Oxidation.

The oxidation of Cr(II) in solutions containing large excesses of bromide was studied by double potential step chronocoulometry. Figure 23 shows the method of analysis of the data and illustrates a typical result. The agreement of the forward and reverse intercepts with each other and with the value measured independently in the supporting electrolyte solution is well within the accuracy of the method. The identity of the forward and reverse slopes shows that the product of the oxidation of Cr(II) under these conditions is entirely CrBr²⁺.

Double potential step chronocoulometry experiments were done in solutions 0.5-3 mF in Cr(II) and with bromide concentrations of 0.878 F, 0.439 F, 0.219 F, 0.110 F, and 0.0549 F. The value of τ was approximately 20 ms., 40 ms., or 80 ms. The initial and final potentials, E₀ and E₂ in Figure 21, were -0.750 v. vs. SCE and the anodic step potential, E₁ in Figure 21, was varied between the anodic limit set by the oxidation of mercury and the cathodic limit (-0.300 v. vs. SCE) set by the irreversibility of Cr(II) oxidation.

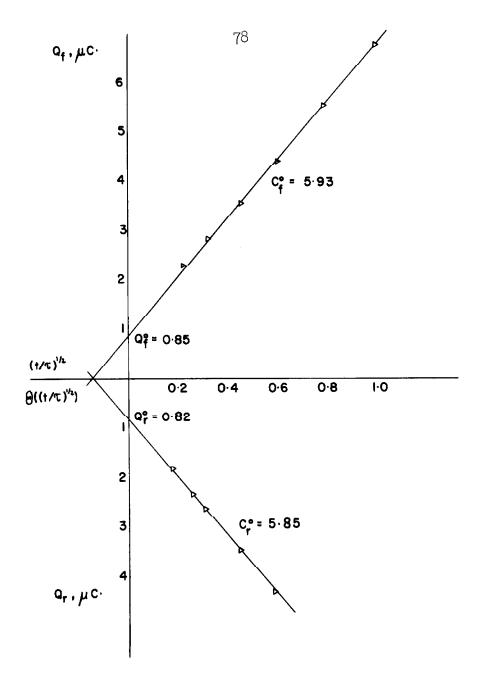


Figure 23. Reduced time function plot of double potential step chronocoulometric behavior for Cr(II) in excess bromide. Solution: 3.15 mF Cr(II) in 0.100 F HClO₄, 0.878 F NaBr (μ = 1.00). E = E₂ = -0.750 v. vs. SCE; E₁ = -0.250 v. vs. SCE. The measured double layer blank is 0.90 μ C. The forward and reverse slopes correspond to Cr(II) concentrations of 2.67 and 2.64 mF, respectively. τ = 0.0385. The difference between the bulk concentration of Cr(II) and that given by the slopes is caused by air oxidation of the Cr(II) solution in the course of the experiment.

In about 30 cases including a suitable coverage of the variation of parameters the Q - t traces obtained were plotted as in Figure 23. There were some deviations from the expected ideal behavior which are discussed below, but none of the experiments for which the Q - $t^{\frac{1}{2}}$ plots were made showed any evidence of failure to form entirely $CrBr^{2^+}$ in the oxidation of Cr(II).

If the charge passed in the forward and reverse steps, Q_f and Q_b , be measured at times τ and 2τ , respectively, as defined in Figure 21, the ratio ${}^*Q_b(2\tau)/{}^*Q_f(\tau)$ should be 0.586 (28). It is assumed that the measured values of Q are corrected for double layer charging by subtracting from them the amount of charge required to charge the double layer, Q_{d1} , measured by duplicating the experiment in the absence of electroactive material. *Q is the double-layer-corrected value of Q.

The use of this criterion for ideality without examining the $Q - t^{\frac{1}{2}}$ behavior is open to a good deal of criticism. The most obvious point is that the slopes and intercepts may vary in such a way that the ratio of charges is 0.586 but neither the slopes nor the intercepts have the correct value.

Over 200 Q - t traces were obtained under 127 different sets of conditions. The average value of the ratio ${}^*Q_b(2\tau)/{}^*Q_f(\tau)$ was found to be 0.585 \pm 0.005. There was no significant variation of the ratio with any of the parameters. These results show that there is complete inclusion of bromide in the oxidation of Cr(II) under conditions where the reaction is sufficiently fast to be diffusion controlled under the conditions of double potential step chronocoulometry and there is a substantial excess of bromide present.

When the bromide concentration is very low we obtain somewhat different and more interesting results. An example is presented in Table 5 which gives results of experiments performed in 1.93 mF bromide solution. The quantities given are those defined by the $Q - t^{\frac{1}{2}}$ plots in Figure 23.

TABLE 5

E ₁ , v. vs. SCE	τ, sec.	Q _{dl} , μC.	Q ^o _f , μC.	Q ₂ °, μC.	C _f , mF	C, mF
-0.300	0.0404	0.50	-0.01	0.46	1.41	1.14
-0.250	0.0402	0.55	0.03	0.42	1.58	1.40
-0.200	0.0398	0.59	0.37	0.46	1.58	1.57
-0.150	0.0400	0.67	0.57	0.58	1.49	1.50
-0.100	0.0400	0.73	0.54	0.57	1.55	1.58
-0.050	0.0401	0.89	0.65	0.65	1.49	1.49

 $A = 0.0409 \text{ cm}^2$

In these experiments the variation in slopes from one experiment to the next and the discrepancy between measured double layer intercept and the intercept from the $Q - t^{\frac{1}{2}}$ plot is rather larger than often observed, but the internal consistency of each experiment is sufficiently good that the results are convincing. From examinations of the intercepts and the slopes (concentrations) it is clear that at -0.300 v. and -0.250 v. the oxidation of Cr(II) is not diffusion controlled and that, furthermore, there is not complete inclusion of bromide, though there is clearly a stoicniometric excess of bromide over Cr(II).

At -0.200 v. and more anodic potentials, however, the oxidation is apparently diffusion controlled, as shown by the agreement of the forward and reverse intercepts and the constancy of the forward slope with potential. Also, there is complete inclusion of bromide, as shown by the identity of the reverse and forward slopes in each case.

Experimental procedures. The equipment used is discussed on page 76.

The cell and general procedures for filling are discussed on page 64.

Experiments were carried out at 27.0° C.

Cr(II) stock solutions were prepared and analyzed as discussed in Chapter 2.

Supporting electrolyte solutions were prepared from $HClO_4$, NaBr, and NaClO₄ solutions prepared as previously described. The concentrations were such that the mixture of supporting electrolyte solution and Cr(II) stock solution giving the desired Cr(II) concentration would have the desired bromide concentration and 0.100 F $IIClO_4$ (μ = 1.00).

The value of $Q_{\rm dl}$ for each set of conditions was measured in the appropriate supporting electrolyte solution just before adding the Cr(II) solution.

Discussion of the data. In many cases the data, while showing no evidence of failure of Cr(II) to be oxidized quantitatively to CrBr²⁺, did not correspond to the ideal double potential step chronocoulometric behavior.

The most common deviation from expected behavior was failure of the forward and reverse intercepts, $Q_{\underline{f}}^{O}$ and $Q_{\underline{b}}^{O}$, to agree with the independently measured value, $Q_{\underline{a}\underline{l}}$. The values of $Q_{\underline{f}}^{O}$ and $Q_{\underline{r}}^{O}$ usually agreed to within a few percent but frequently differed from $Q_{\underline{d}\underline{l}}$ by 10% or more.

A second and apparently independent phenomenon was the tendency for the forward intercept to be larger than the reverse intercept and the forward slope to be less than the reverse slope. These two effects appear together; the greater the difference in intercepts, the greater the difference in slopes.

These characteristics do not always appear, but do appear repeatedly. They have been observed in similar experiments with 0.5 mF Cd(II) in 1 F NaNO₃ solution. We feel that these anomalous results require a pertinent warning to the experimenter but have no bearing on the validity of our conclusions (31).

3. Discussion.

The chronocoulometric results confirm and add detail to the conclusions of the chronopotentiometric experiments. At potentials more anodic than -0.300 v. vs. SCE and bromide concentrations higher than 0.055 F, Cr(II) is quantitatively oxidized to CrBr²⁺. Therefore under these conditions Cr(II) is oxidized by a bromide bridge mechanism.

The chronopotentiometric result that $CrBr^{2+}$ is not quantitatively formed on Cr(II) oxidation at cathodic potentials even in excess bromide is confirmed by the chronocoulometric experiments.

These results are predicted by the theory of parallel reactions for potential step chronocoulometry. When the anodic step is applied

two reactions take place; the oxidation of Cr(II) via a bromide bridge to form the product CrBr²⁺, and the oxidation of Cr(II) by the mechanism prevailing in the absence of bromide to form Cr³⁺. These two reactions have different kinetic parameters and are isolated from each other by the lack of equilibrium between the products.

A detailed general mathematical description of this situation is presented in Appendix II. The qualitative result is that when the rates for the two processes are comparable both products are formed, in amounts roughly proportional to their respective rates. The rate parameters for the two processes were determined and are discussed in Part III. These constants were used with the equations of Appendix II to calculate the expected product distribution for the potential step oxidation of Cr(II) in the presence of excess bromide. It was found that when the oxidation of Cr(II) is sufficiently fast that diffusion control is attained, the product of the reaction should be entirely CrBr²⁺; but, when the bromide concentration is sufficiently low, and the potential sufficiently cathodic, some Cr³⁺ should be formed.

Double potential step chronocoulometric verification that an amount of ${\rm CrBr}^{2^+}$ is formed which corresponds to the fraction of ${\rm Cr}({\rm II})$ oxidized via bromide under conditions where less than 100% of the ${\rm Cr}({\rm II})$ occurs via the bromide-dependent path has little chance of success. The algebraic complexity of the equations for parallel reactions isolates the observable quantities from the parameters of interest so effectively that convincing agreement between measured and calculated amounts of ${\rm CrBr}^{2^+}$ formed surely would not be obtained.

Chapter 6

THE OXIDATION OF CHROMIUM(II) IN THE PRESENCE OF IODIDE: RATE COMPETITION WITH CHLORIDE

In Chapter 5 we discussed the competition between the electrode reactions

$$Cr^{2^+} + Br^- \xrightarrow{-e^-} CrBr^{2^+}$$
 (la)

$$\operatorname{Cr}^{2^+} \xrightarrow{-e} \operatorname{Cr}^{3^+}$$
 (1b)

and its effect on the ratio of products formed. In that case the effect was seen as a nuisance. However, if one of the reactions of interest is the now well-characterized oxidation of Cr(II) via a chloride bridge, and the other the oxidation of Cr(II) via another halide bridge, the chloride-assisted reaction may be used as a probe to determine how the other reaction proceeds.

This approach is especially attractive in the case of iodide. The rate of aquation of CrI^{2^+} is sufficiently large that any technique for finding the amount of CrI^{2^+} formed in the electrochemical oxidation of $\operatorname{Cr}(\operatorname{II})$ in the presence of iodide must have a characteristic time of a second or less. However, double potential step chronocoulometry is not applicable because in iodide solutions $\operatorname{Cr}(\operatorname{II})$ oxidation and mercury oxidation are not well separated. This problem occurs at all iodide concentrations because although lowering the iodide concentration moves the mercury oxidation to a more anodic potential it also decreases the rate of $\operatorname{Cr}(\operatorname{II})$ oxidation so that a greater overpotential is required for diffusion control.

The use of the chloride bridged oxidation of Cr(II) as a probe removes this difficulty, for an electrolysis can be carried out under diffusion controlled conditions and the long lived product, CrCl²⁺, will record the reaction path.

I. Cyclic Voltammetry of Cr(II) in Iodide Solutions

At low iodide concentrations the oxidation of Cr(II) is sufficiently separated from the depolarization of mercury that cyclic voltammetry at slow sweep rates may be used to study the reaction qualitatively. Figures 24-28 illustrate the behavior observed. In each case the sweep was begun at -0.700 v. vs. SCE with the first half-cycle anodic; the cathodic limit of the sweep was approximately -1.20 v. vs. SCE.

Figure 24 shows the general features in a solution with a slight excess of iodide. The calculated flux ratio is 1.00, but there is a slight excess of iodide because of the air oxidation of Cr(II). The peak A corresponds to the oxidation of Cr(II) by the iodide path, B to the reduction of CrI²⁺, and C to the reduction of Hg₂I₂ (or some other mercury species). The identification of C is clearly established by comparison with the background in the solution containing iodide alone.

The succeeding figures show the effect of increasing the Cr(II) concentration. Taken together, these voltammograms show the following characteristics. The peak at A remains in the same position and does not change in height as the Cr(II) concentration is increased. Therefore it must be iodide diffusion controlled. The fact that the cathodic peak B maintains its position and height as the Cr(II) concentration is in-

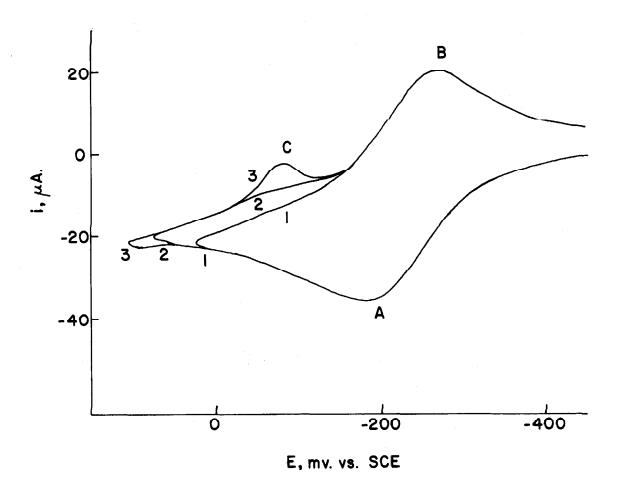


Figure 24. Cyclic voltammetry of Cr(II) in iodide solution. Solution: 1.30 mF NaI, 0.100 F HClO₄ (μ = 1.00) with $D_{\rm Cr}^{\frac{1}{2}}({\rm Cr}(II))/D_{\rm I}^{\frac{1}{2}}(I^-)$ = 1.00. See text for discussion.

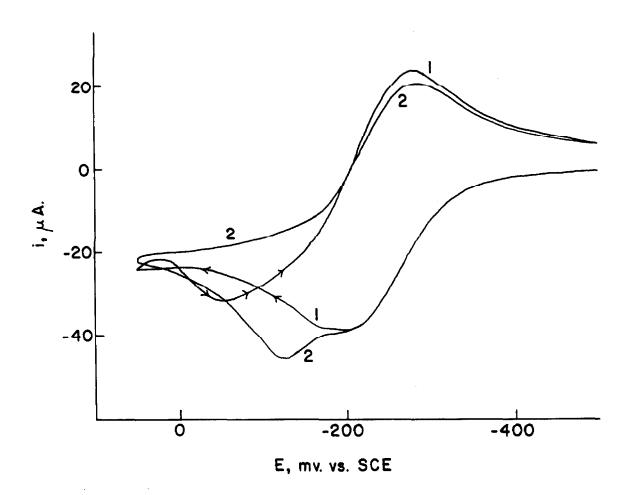


Figure 25. Cyclic voltammetry of Cr(II) in iodide solution. Solution: 1.28 mF NaI, 0.100 F HClO₄ (μ = 1.00) with $D_{\rm Cr}^{\frac{1}{2}}({\rm Cr}({\rm II}))/D_{\rm I}^{\frac{1}{2}}({\rm I}^-)$ = 1.51.

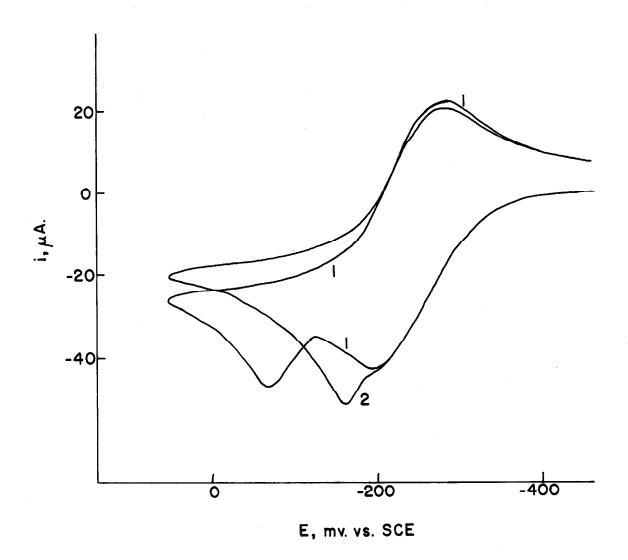


Figure 26. Cyclic voltammetry of Cr(II) in iodide solution. Solution: 1.28 mF NaI, 0.100 F HClO₄ (μ = 1.00) with $D_{Cr}^{\frac{1}{2}}(Cr(II))/D_{I}^{\frac{1}{2}}(I^{-})$ = 1.76.

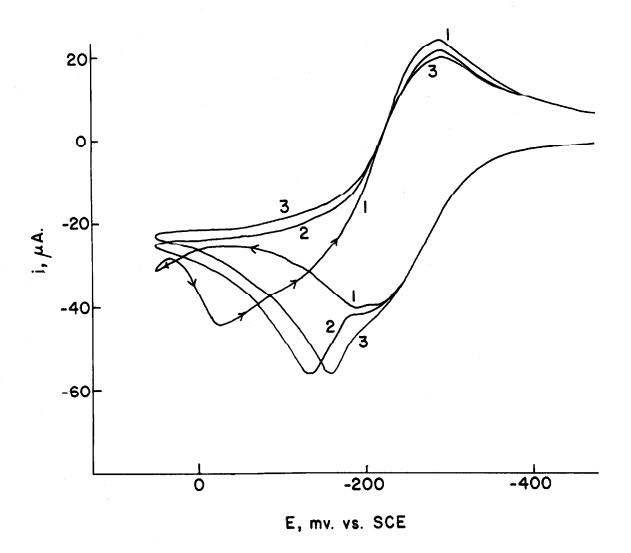


Figure 27. Cyclic voltammetry of Cr(II) in iodide solution. Solution: 1.27 mF NaI, 0.100 F HClO₄ (μ = 1.00) with $D_{Cr}^{\frac{1}{2}}(Cr(II))/D_{I}^{\frac{1}{2}}(I^{-})$ = 2.03.

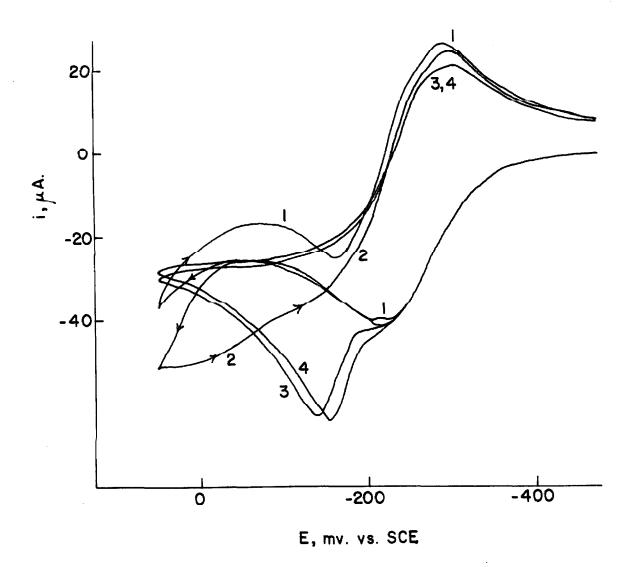


Figure 28. Cyclic voltammetry of Cr(II) in iodide solution. Solution: 1.25 mF NaI, 0.100 F HClO₄ (μ = 1.00) with D_{Cr} (Cr(II))/ D_I $\frac{1}{2}$ (I⁻) = 2.50.

creased confirms the diagnosis that it is due to the reduction of the product of A (CrI^{2+}) .

In excess Cr(II) solutions a second anodic peak appears whose height increases with increasing Cr(II) concentration and whose position is heavily dependent on the number of the cycle. The irreproducibility from the first to succeeding cycles is a phenomenon which we cannot explain. In each case the last cycle shown is the steady state behavior. This behavior is independent of the age of the drop in the solution, or whether the drop has been used before. It is also remarkably reproductible from one trial to the next.

The constant height and position of the anodic peak A and cathodic peak B at constant iodide concentration and varying excess Cr(II) is convincing evidence that Cr(II) is oxidized via an iodide bridge to form CrI²⁺.

Experimental details. These experiments were carried out using the cell described on page 65 and the multipurpose instrument described on page 76. The voltammograms were recorded using a Moseley Autograph X-Y recorder. The sweep rate was 0.134 v./sec.

II. Controlled Potential Electrolysis of Chromium(II) Solutions: Oxidation in the Presence of Chloride-Iodide Mixtures

The oxidation of Cr(II) in the presence of chloride-iodide mixtures presents the intriguing possibility that the product distribution might differ from that predicted by the parallel reaction theory because iodide is adsorbed on mercury to a greater extent than is chloride. To investigate this possibility, large-scale electrolyses similar to those described in Chapter 3 were carried out in solutions containing both iodide and chloride.

The oxidations were done at -0.192 v. vs. SCE instead of at -0.012 v. vs. SCE to avoid oxidation of mercury. The product solutions were analyzed for the amount of iodide and for the total amount of free halide by potentiometric titration with standard silver solution. The amount of CrCl²⁺ formed was found by difference. The initial conditions and the amount of free chloride found in the product solutions are given in Table 6. In each experiment the initial chloride to iodide ratio was about 10.

The results are presented in Figure 29. The slope of the line defined by the experimental points is 0.75 meq.CrCl²⁺/meq.Cr(II). In the three experiments with the largest Cr(II) concentrations the difference between the amount of CrCl²⁺ formed and the amount that would have been formed had no iodide been present is greater than the amount of iodide. This is possible because the time required for electrolysis (about one hour) is long compared with the lifetime of CrI²⁺, so that iodide is being freed at a rate commensurate with its use.

There is no point in attempting even an approximate treatment of the problem of mass transfer to a stirred mercury pool electrode. However, the results of Appendix II suggest that the fraction of CrCl^{2^+} formed in these experiments should be approximately equal to the ratio of the rate of formation of CrCl^{2^+} to the sum of the rates for all possible oxidation paths.

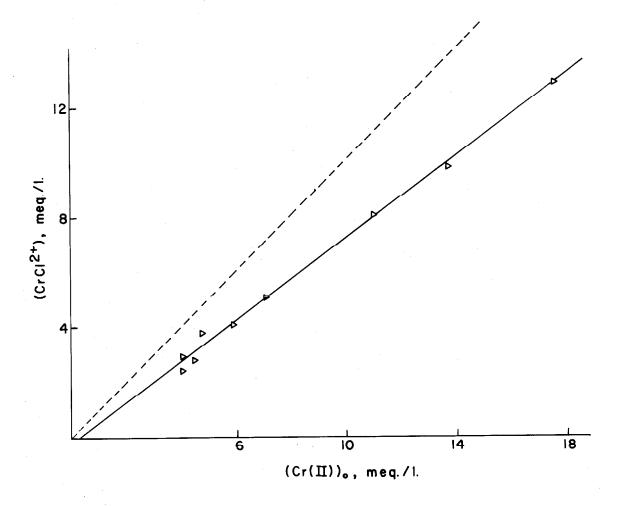


Figure 29. The effect of iodide on the inclusion of chloride in the controlled potential oxidation of Cr(II). The dotted line shows the behavior to be expected in the absence of iodide. See Table 6 for conditions.

TABLE 6

Controlled Potential Electrolysis of Cr(II) Solutions
Containing Chloride and Iodide

(I ⁻) _{,1}	(cl ⁻) _i	(CrII) _o	(Cl ⁻) _f
0.1008	1.007	0.3010	0.798
tf	11	0.7020	0.506
0.0978	1.018	0.9007	0.357
11	п	0.5199	0.636
11	11	0.1753	0.892
11	11	0.2074	0.856
††		0.1747	0.915
- H	11	0.1922	0.897

i refers to initial amounts

f refers to free chloride found after electrolysis $(CrII)_{O}$ is the value obtained from the integrator for the amount of $Cr(\Pi)$ oxidized electrochemically.

All figures are given in total number of milliequivalents of material in the solution. The solution volume in these experiments varied from 42 to 50 ml.

From Figure 2 of Reference 6 we can extract the following rate constants for the oxidation of Cr(II) at -0.192 v. vs. SCE:

$$k_1 = 0.14 \times 10^{-2} \text{ cm./sec.}$$
 $(C1^-)k_2 = 2.73 \times 10^{-2} \text{ cm./sec.}$
 $(I^-)k_2 = 6.40 \times 10^{-2} \text{ cm./sec.}$
 $(C1^-) = (I^-) = 5 \times 10^{-6} \text{ moles/cm.}^3$

Here k_1 is the rate constant in the absence of bridging ligands and $(Cl^-)k_2$ and $(l^-)k_2$ are the pseudo-first-order rate constants in the presence of chloride and iodide, respectively, for the ligand bridged path alone.

For the experiments described above the value of the rate ratio is

$$\frac{(\text{Cl}^-)k_2}{(\text{Cl}^-)k_2 + (\text{I}^-)k_2 + k_1} = 0.74 \pm 0.03$$
 (2)

In calculating this ratio it was assumed that the iodide concentration is equal to its initial value, $(I^-)_i$, given in Table 6, and that the chloride concentration is equal to $\frac{2}{3}(Cl^-)_f + \frac{1}{3}(Cl^-)_i$, which is approximately the average value of the chloride concentration during the electrolysis.

The value of the ratio given in Equation 2, 0.74, is in remarkable agreement with the value of 0.75 given by the slope of the line in Figure 29. This agreement between experiment and the prediction of parallel reaction theory suggests that the influence of halide adsorption on the mechanism is contained in the rates themselves. The mechanistic implications of the rate parameters are discussed in Chapter 7.

Experimental procedures. The general procedures and equipment used are described in Chapter 3.

The product solutions were made 5% in Ba(ClO₄)₂ before analysis to suppress the adsorption of silver ion on precipitated silver iodide. Analysis of standard chloride-iodide mixtures showed that the determination is capable of 0.2% accuracy in chloride determination when the

chloride to iodide ratio is 10:1. The accuracy drops with decreasing chloride to iodide ratio.

Several blanks were done in which all components except the Cr(II) were added to the cell, the solution was electrolyzed at -0.192 v. vs. SCE for about one hour, and then analyzed for chloride. A maximum of 0.001 milliequivalent of current was passed; the chloride analysis was 0.5% low.

Chapter 7

THE RATE OF OXIDATION OF CHROMIUM(II)

The role of bridging ligands in the oxidation of Cr(II) at mercury electrodes can be studied by determining the effect that those ligands have on the rate of the oxidation. There are two ways in which the determination of rates helps to define the mechanism. First, the dependence of the pseudo-first-order heterogeneous rate constant for the reaction on the ligand concentration can be determined. Second, the rate parameters for different ligands can be compared and the differences in rate correlated with differences in the properties of the ligands.

The theory of electrode kinetics is discussed by Delahay (32). The general equation describing the rate of an electrode reaction is

$$\frac{i(t)}{n \Im AD} = k_h^o \left[C_O(0,t) e^{-\alpha \frac{n\Im}{RT} (E-E^o)} - C_R(0,t) e^{(1-\alpha) \frac{n\Im}{RT} (E-E^o)} \right]$$
 (1)

When the reaction is sufficiently irreversible, one of the terms in the right hand side of Equation 1 may be neglected and data are easily analyzed without prior knowledge of the standard potential, E^{O} , although the standard potential must be known to evaluate the standard rate constant, k_h^{O} . When the reaction is quasi-reversible both terms must be considered. This increases the complexity of the relationship between the rate and the rate parameters, and requires that E^{O} be known independently, since it is used in the analysis.

The rate parameters for a reaction are usually found by studying a reduction rate, sometimes an oxidation rate, rarely both. However, if

rate parameters are determined for both the anodic and cathodic processes and they agree with each other, the results are much more convincing than those based on a single determination.

I. <u>Kinetic Parameters for the Couple Cr(II)/Cr3+</u> in Perchlorate Solutions

In the absence of bridging ligands the $\mathrm{Cr}(\mathrm{II})/\mathrm{Cr}^{3^+}$ couple is highly irreversible at mercury electrodes. This means that simple techniques can be used to measure the rates and the kinetic parameters are easily extracted from the measured rates. We have measured the rate of oxidation of $\mathrm{Cr}(\mathrm{II})$ and the rate of reduction of Cr^{3^+} and have determined the rate parameters for each reaction.

1. The Rate of Reduction of Cr3+.

We have measured the rate of reduction of Cr^{3^+} polarographically. The data were analyzed by straightforward application of the theory of totally irreversible polarographic waves (33). Semi-logarithmic plots of $f(i/i_d) = (12t/7)^{\frac{1}{2}} \lambda$ vs. potential are shown in Figure 30. The derived rate parameters are presented in Table 7. The scatter in results is well within that typically observed in electrochemical rate measurements.



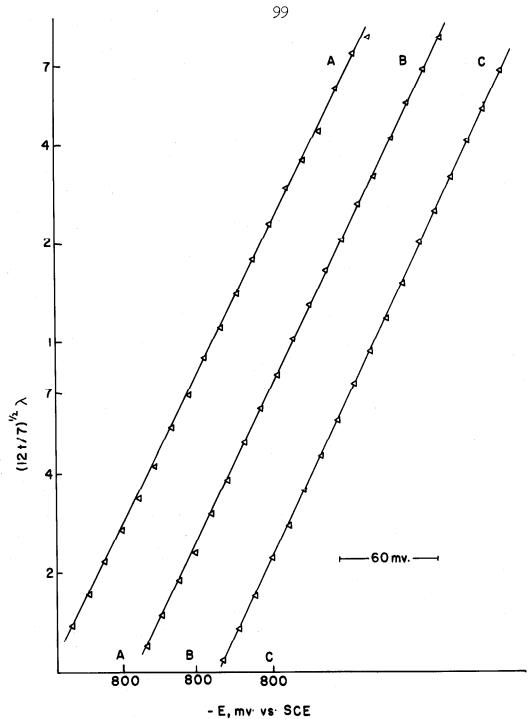


Figure 30. Semi-logarithmic plot of λ as a function of potential for the polarographic reduction of $\text{Cr}^{3^{\dagger}}$. Solutions:

A, 0.712 mF Cr^{3+} , 0.0728 F HClo_4 ($\mu = 0.98$);

B, 1.420 mF Cr^{3+} , 0.0797 F HClo_4 (μ = 1.00);

C, 2.12 mF Cr^{3+} , 0.0868 F $HClo_4$ ($\mu = 1.01$).

TABLE 7

(Cr ³⁺),mM	$k_h^0 \times 10^5$, cm./sec.	α
0.71	0.86	0.61
1.42	0.66	0.62
2.12	0.55	0.64
Av.	0.69 <u>+</u> 0.11	0.62 + 0.01

 $E^{\circ} = -0.650 \text{ v. vs. SCE}$

Experimental procedures. Digital polarograms were obtained using a three-electrode polarograph and recorded with a Brown millivolt recorder.

Solutions were prepared by adding a measured volume of Cr(III) stock solution (prepared as described in Chapter 2) to a measured volume of supporting electrolyte solution with 0.066 F HClO₄ and 0.908 F NaClO₄. The background current was measured in the deaerated supporting electrolyte solution before adding the Cr(III) solution.

A drop knocker was used with the dropping mercury electrode to maintain a drop time of 4 sec. The reference electrode was a Beckman SCE connected to the solution by a cracked glass bead salt bridge containing 1 F NaNO3. The auxiliary electrode was a platinum wire.

2. The Rate of Oxidation of Cr(II).

The rate of oxidation of Cr(II) was measured using potential step chronocoulometry (34). For irreversible oxidations the charge-time relationship for potential step chronocoulometry is

*Q =
$$\frac{K}{\lambda^2} \left(\exp(\lambda^2 t) \operatorname{erfc}(\lambda t^{\frac{1}{2}}) + \frac{2\lambda t^{\frac{1}{2}}}{\sqrt{\pi}} - 1 \right)$$
 (2)

$$K = -n \Im Ak_h^{\circ} C^{\circ} e^{(1-\alpha) \frac{n \Im}{RT} (E-E^{\circ})}$$
(3)

$$\lambda = \frac{k_{h}^{O}}{D^{\frac{1}{2}}} c \qquad (1-\alpha) \frac{n \Im}{RT} (E-E^{O})$$
(4)

 $*Q = Q - Q_{dl}$ is the charge due to faradaic reaction alone. The total measured charge, Q, includes the charge Q_{dl} required to charge the double layer from the initial potential where no reaction takes place to the final potential.

For a diffusion controlled reaction, the charge is

$$*Q_{\bar{d}} = \frac{2n\Im\Delta\bar{D}^{\frac{1}{2}}C^{O}}{\sqrt{\pi}} t^{\frac{1}{2}}$$
(5)

$$*Q_{d} = \frac{2}{\sqrt{\pi}} \frac{K}{\lambda} t^{\frac{1}{2}}$$
 (6)

Substituting Equation 6 into Equation 2 we obtain

$$\frac{2}{\sqrt{\pi}} \left(1 - \frac{*_{Q}}{*_{Q_{d}}} \right) = \frac{1}{\lambda t^{\frac{2}{2}}} \left(1 - \exp(\lambda^{2} t) \operatorname{erfc}(\lambda t^{\frac{1}{2}}) \right)$$
 (7)

A working curve was constructed from calculated values of the function

$$f(\lambda t^{\frac{1}{2}}) - \frac{1}{\lambda t^{\frac{1}{2}}} \left(1 - \exp(\lambda^2 t) \operatorname{erfc}(\lambda t^{\frac{1}{2}}) \right)$$
 (8)

which are presented in Table 8. From this working curve values of $\lambda t^{\frac{1}{2}}$ were obtained for various values of $^*Q/^*Q_d$. This method of determining kinetic parameters is analogous to that used in polarography.

Q-t traces were obtained over 40 msec. intervals for potentials from -0.300 v. to -0.050 v. vs. SCE. Q-t traces were obtained at +0.200 v. vs. SCE to give *Q_d as a function of time. The plots obtained from derived values of $\lambda t^{\frac{1}{2}}$ are shown in Figure 31. The values of the rate parameters obtained from these plots are given in Table 9.

TABLE 9

t, mscc.	k ^O x 10 ⁵ , cm./sec.	α
10	8.4	0.72
20	5.1	0.69
30	2.9	0.67
40	1.8	0.64

$$E^{\circ} = -0.650 \text{ y. ys. SCE}$$

The trend to higher values of the standard rate constant and transfer coefficient at shorter times is probably due to uncertainty in the double layer correction. The longer the time, the smaller $Q_{\rm dl}$ is in comparison with *Q and the smaller the effect of an error in $Q_{\rm dl}$. Both $Q_{\rm dl}$ and *Q are potential dependent, but *Q increases faster with more anodic potential than $Q_{\rm dl}$ does, so error in $Q_{\rm dl}$ affects the transfer coefficient as well as the standard rate constant. The kinetic parameters obtained from the data at 40 msec. are probably closest to the true values.

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TABLE 8 $f(x) = \frac{1}{x}[1 - \exp(x^2)\operatorname{erfc}(x)]$

Х	f(x)	х	f(x)
0.0001	1.1300	0.24	0.9257
0.0002	1.1289	0.25	0.9186
0.0005	1.8804	0.26	0.9116
0.001	1.1276	0.27	0.90148
0.002	1.1265	0.28	0.8980
0.005	1.1234	0.29	0.8913
0.01	1.1184	0.30	0.8847
0.02	1.1087	0.31	0.8781
0.03	1.0990	0.32	0.8717
0.04	1.0896	0.33	0.8653
0.05	1.0802	0.34	0.8591
0.06	1.0710	0.35	0.8529
0.07	1.0619	0.36	0.8468
0.08	1.0530	0.37	0.8407
0.09	1.0441	0.38	0.8347
0.10	1.0354	0.39	0.8288
0.11	1.0268	0.40	0.8230
0.12	1.0184	0.41	0.8173
0.13	1.0101	0.45	0.7950
0.14	1.0018	0.50	0.7686
0.15	0.9938	0.55	0.7458
0.16	0.9858	0.60	0.7203
0.17	0.9779	0.70	0.6772
0.18	0.9701	0.80	0,6386
0.19	0.9625	0.90	0.6038
0.20	0.9549	1.00	0.5724
0.21	0.9474	1.10	0.5439
0,22	0.9401	1.20	0.5179
0.23	0.9328	1.30	0.4941

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TABLE 8--Continued

х	r(x)	Х	f(x)
1.35	0.4830	4.2	0.20695
1.40	0.4723	4.4	0.19883
1.50	0.4523	4.6	0.19132
1.60	0.4338	4.8	0.18435
1.70	0.4167	5.0	0.17786
1.80	0.4008	5.2	0.17181
1.90	0.3860	5.4	0.16615
2.0	0.3723	5.6	0.16086
2.1	0.3595	5.8	0.15588
2.2	0.3474	6.0	0.15120
2.3	0.3362	6.2	0.14680
2.4	0.3256	6.4	0.14264
2.5	0.3157	6.6	0.13871
2.6	0.3063	6.8	0.15498
2.7	0.29745	7.0	0.13146
2.8	0.28909	7.4	0.12492
2.9	0.28117	7.8	0.11901
3.0	0.27366	8.2	0.11362
3.1	0.26654	8.6	0.10870
3.2	0.25977	9.0	0.10419
3.4	0.24720	9.5	0.09905
3.6	0.23576	10.0	0.09439
3.8	0.22532		
4.0	0.21575		



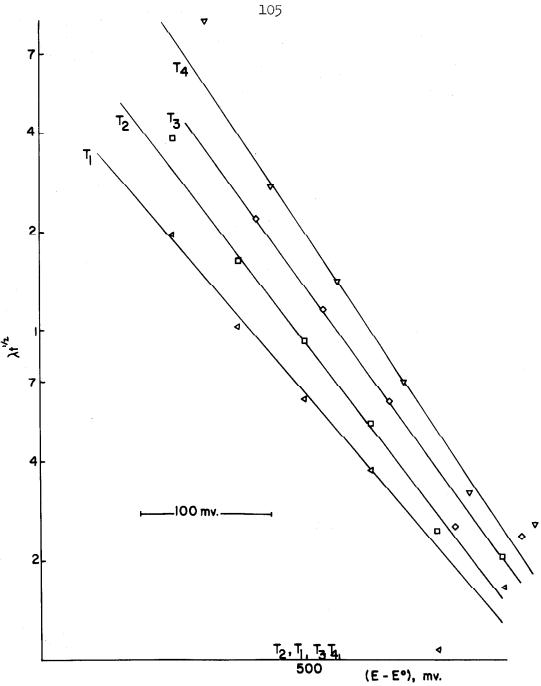


Figure 31. Semi-logarithmic plot of $\lambda t^{\frac{1}{2}}$ as a function of potential for the potential step chronocoulometric oxidation of Cr(II). Solution: 1.09 mF Cr(II), 0.100 F HClO₄ (μ = 1.00). The letters refer to the measurement time for each set of points: T_1 , 10 ms.; T_2 , 20 ms.; T_3 , 30 ms.; T_4 , 40 ms.

Experimental details. The experiments were carried out as described on page 100. Solutions were 0.5 mF Cr(II), 0.100 F HClO₄ (μ = 1.00).

The rate of oxidation of Cr(II) in solutions 0.5-7.0 mF in Cr(II), 0.1-0.01 F in HClO₄, and 1 F in NaClO₄ was determined by Aikens and Ross (6) using a potentiostatic technique. They extrapolated 1 vs. $t^{\frac{1}{2}}$ to give the intercept $i_0 = kn \% AC$, where the equation defines their value of k. We have plotted their rate data (Figure 32) to obtain the rate parameters $k_h^0 = 0.78 \times 10^{-5}$ cm./sec. (E⁰ = -0.650 v. vs. SCE) and $\alpha = 0.63$.

3. Discussion.

The best values of the rate parameters for the couple ${\rm Cr}^{2^+}/{\rm Cr}^{3^+}$ are given in Table 10. The agreement among these values is quite good.

When the transfer coefficient for an electrochemical reaction is 0.5 the rate of the reaction as a function of potential is symmetrical about the standard potential for the couple. The pronounced asymmetry observed if $\alpha \neq 0.5$ is illustrated by the normalized polarogram shown in Figure 33. The polarogram was calculated using the values $k_h^0 = 10^{-5}$ cm./sec. and $\alpha = 0.63$.

TABLE 10

$k_h^{o} \times 10^5$, cm./sec.	α	Reference
0.69	0.62	Table 8
1.8	0.64	Table 9
0.78	0.63	Reference 6

 $E^{\circ} = -0.650 \text{ v. vs. SCE}$

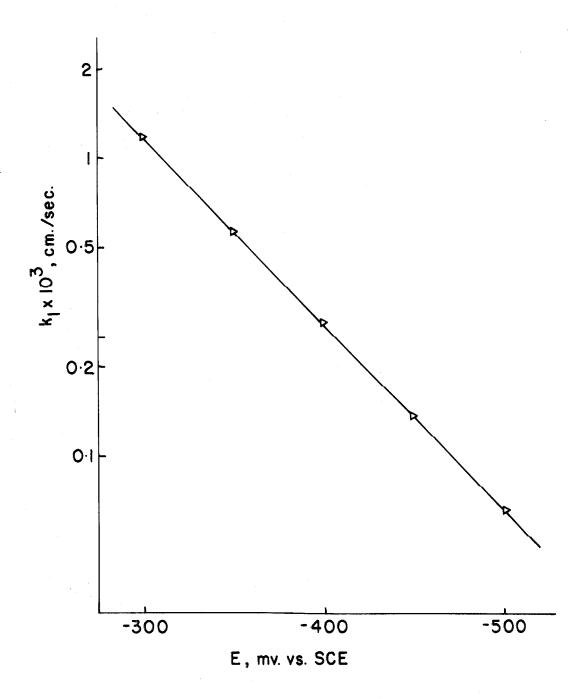


Figure 32. Semi-logarithmic plot of the potential dependence of the rate of the reaction $\operatorname{Cr}^{2^+} \to \operatorname{Cr}^{3^+} + \operatorname{e}^-$ from the data of Aikens and Ross (6).

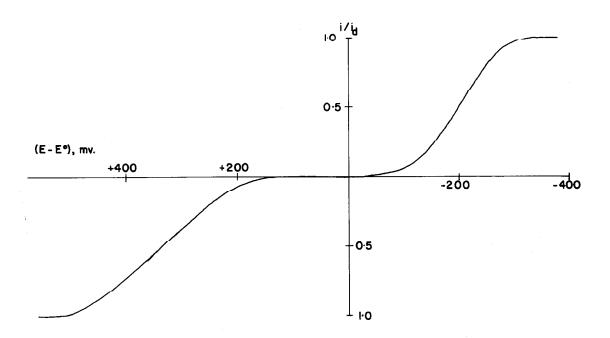


Figure 33. Normalized polarogram for the kinetic parameters $k_h^0 = 10^{-5}$ cm./sec. and $\alpha = 0.63$ with n = 1, $D^{\frac{1}{2}} = 0.00254$, $T = 27^{\circ}$ C.

II. Kinetic Parameters for the Couple Cr(II)/CrCl2+

Aikens and Ross (6) present data which can be used to obtain the kinetic parameters for the reaction

$$\operatorname{Cr}^{2^+} + \operatorname{Cl}^- \xrightarrow{-e^-} \operatorname{Cr}\operatorname{Cl}^{2^+} \tag{9}$$

We cannot calculate the standard rate constant because the standard potential is not known. However, from the plot of this data shown in Figure 34 we obtain the value of the transfer coefficient, $\alpha = 0.43$. This is in contrast to the value of 0.63 for the reaction

$$\operatorname{Cr}^{2^+} \xrightarrow{-e^-} \operatorname{Cr}^{3^+}$$
 (10)

From unpublished rate data obtained by Aikens and Ross (35) we derive the value $\alpha = 0.39$ for the reduction of CrCl^{2^+} in perchlorate solution at pH 2 ($\mu = 1.00$). From similar data for reduction of Cr^{3^+} (35) we extract the value $\alpha = 0.62$ (cf. Table 10), which supports the validity of the method and indicates that the difference between the transfer coefficients for Cr^{3^+} reduction and CrCl^{2^+} reduction is real.

III. Kinetic Parameters for the Couple Cr(II)/Cr(III) in Bromide Solution

In bromide solution under conditions where the oxidation of Cr(II) is not diffusion limited, the oxidation takes place via two paths,

$$Cr^{2^+} + Br^- \xrightarrow{-e^-} CrBr^{2^+}$$
 (11a)

$$\operatorname{Cr}^{2^{+}} \xrightarrow{-e^{-}} \operatorname{Cr}^{3^{+}}$$
 (11b)

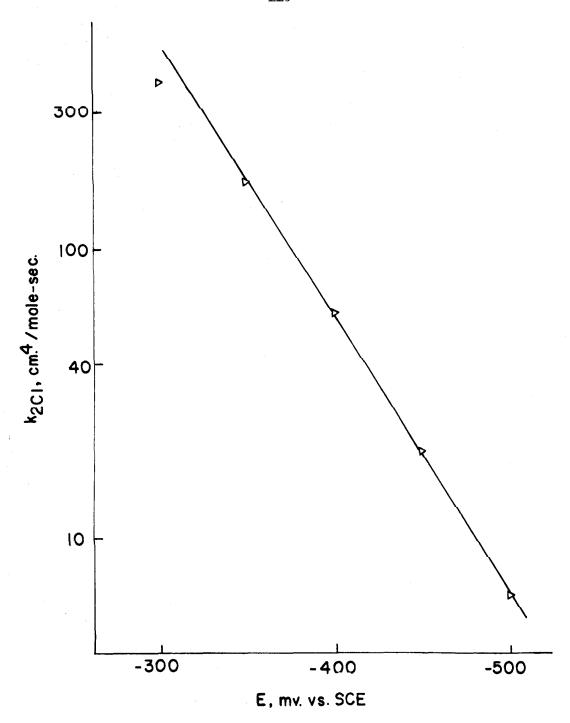


Figure 34. Semi-logarithmic plot of the potential dependence of the rate of the reaction $\text{Cr}^{2^+} + \text{Cl}^- \rightarrow \text{CrCl}^{2^+} + \text{e}^-$ from the data of Aikens and Ross (6).

as has been discussed above (page 82).

To determine the kinetic parameters for the bromide-dependent process we must measure the combined rate as a function of bromide concentration and extract from those data the bromide-dependent part of the rate.

The situation is slightly different for the cathodic process:

$$\operatorname{CrBr}^{2^{+}} \xrightarrow{+e^{-}} \operatorname{Cr}^{2^{+}} + \operatorname{Br}^{-} \tag{12a}$$

$$\operatorname{Cr}^{3^{+}} \xrightarrow{+e^{-}} \operatorname{Cr}^{2^{+}}$$
 (12b)

because the reduction of $CrBr^{2^+}$ is diffusion controlled under most conditions at potentials anodic of Cr^{3^+} reduction. This means that the rate of Reaction 12a can be measured directly without interference from Reaction 12b.

1. Chronopotentiometric Measurement of the Rate of Oxidation of Cr(II) in Dilute Bromide Solution.

The rate of oxidation of Cr(II) in 1 mF NaBr solution was determined chronopotentiometrically at a hanging mercury drop electrode.

The chronopotentiograms were analyzed as totally irreversible waves. The potential-time relation is obtained by substituting the chronopotentiometric equation for $C_R(0,t)$ (36) in Equation 1 with $C_O(0,t)=0$, giving

$$E = E^{\circ} - \frac{RT}{(1-\alpha)n\%} \ln \frac{k_{h}^{\circ} r_{o}}{D} - \frac{RT}{(1-\alpha)n\%} \ln \left[\exp \left(\frac{Dt}{r_{o}^{2}} \right) \operatorname{erfc} \left(\frac{(Dt)^{\frac{1}{2}}}{r_{o}} \right) - \exp \left(\frac{D\tau}{r_{o}^{2}} \right) \operatorname{erfc} \left(\frac{(D\tau)^{\frac{1}{2}}}{r_{o}} \right) \right]$$

$$(13)$$

The calculation of the time-dependent term is more readily done by expanding the argument of the logarithm in power series. This removes some of the dependence on the diffusion coefficient, D, and the radius of the electrode, $r_{\rm o}$. Only three terms of the expansions need be taken. The resulting equation is

$$E = E_{o} - \frac{RT}{(1-\alpha)n\Im} \ln \frac{2 k_{h}^{o}}{\sqrt{\pi D}} - \frac{RT}{(1-\alpha)n\Im} \ln \left[(\tau^{\frac{1}{2}} - t^{\frac{1}{2}}) - \frac{\sqrt{\pi}}{2} \frac{D^{\frac{1}{2}}}{r_{o}} (\tau - t) + \frac{2}{3} \frac{D}{r_{o}^{2}} (\tau^{\frac{3}{2}} - t^{\frac{3}{2}}) \right]$$
(14)

A logarithmic plot of a chronopotentiogram according to this equation is shown in Figure 35. The derived values of the kinetic parameters are $\alpha=0.50$ and $k_h=1.25 \times 10^{-6}$ cm./sec., where the rate constant is referred to E = 0 v. vs. SCE. A similar plot for another chronopotentiogram gave the values $\alpha=0.45$ and $k_h=0.72 \times 10^{-6}$ cm./sec.

Experimental details. The chronopotentiograms were obtained as described on pp. 64ff.

The experimental solution had 1.69 mF Cr(II), 0.100 F HClO₄, 1.00 mF NaBr (μ = 1.00).

Transition times were about 2.3 sec.

2. Polarographic Determination of the Bromide Dependence of the Rate of Cr(II) Oxidation.

The rate of oxidation of Cr(II) in solutions with varying bromide concentration was determined polarographically. At large bromide concentrations the rate is sufficiently large that the quasi-reversible analy-

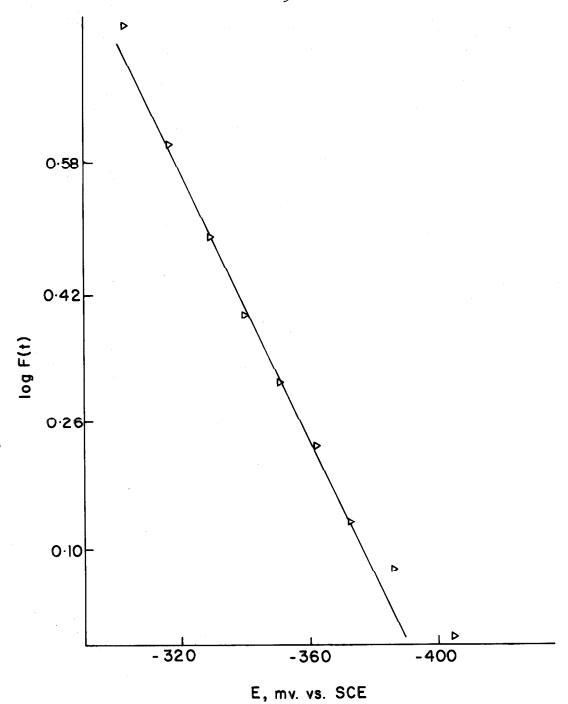


Figure 35. Chronopotentiometric determination of the rate of Cr(II) oxidation in dilute bromide solution. Solution: 1.7 mF Cr(II), 1.01 mF NaBr, 0.100 F HClO $_4$ (μ = 1.00). The data is plotted according to Equation 14. F(t) is the argument of the second logarithmic term in that equation.

sis must be used. The method is discussed in detail by Delahay (37). The value of the effective half-wave potential for use in the analysis was determined by the extrapolation procedure of Koryta (38) which is illustrated below in Figure 38.

When the points used in the analysis of the polarograms are 0.120 v. or more from the half-wave potential, the backward reaction contributes less than 1% of the current. For all but the two highest bromide concentrations, the totally irreversible analysis was used for the polarograms by selecting only points near the head of the wave as far from the half-wave potential as possible. The values of α obtained from the semi-logarithmic plots of rate vs. potential for each bromide concentration are given in Table 11.

TABLE 11

(Br ⁻),moles/1.	α
0.874	0.29
0.436	0.28
0.0546	0,28
0.00192	0.27
0.00154	0.49
0.00106	0.49

Figure 36 shows the bromide dependence of the rate at several different potentials. These results show that the pseudo first order heterogeneous rate constant for the oxidation of Cr(II) in the presence of bromide can be written in the form $k = k_1 + k_2(Br)$. From the slopes of the lines in Figure 36 we obtain the constant for the bromide dependent path, k_2 , and the intercepts give k_1 .

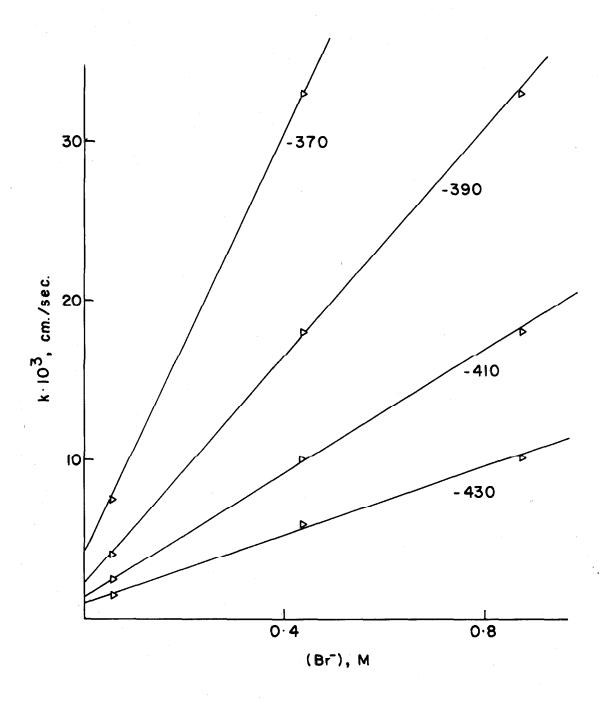


Figure 36. The variation of the rate of Cr(II) oxidation with bromide concentration. The numbers on the lines are the potentials at which the rate was measured. See Page 116 for conditions.

The semi-logarithmic plot in Figure 37 shows the potential dependence of k_2 . From this plot we obtain the transfer coefficient $\alpha = 0.21$. The rate constant is $k_h^0 = 1.82$ cm. 4 /mole.sec. referred to E = -0.500 v. vs. SCE. The logarithm of the k_1 values obtained from the intercepts do not show a linear dependence on the potential. The uncertainty in these values is so large that such a relationship could hardly be expected. However, the values are all within a factor of 2 of the rates calculated from the α values and standard rate constants given in Table 10.

Experimental details. The polarograms were obtained with a Sargent Model XV Polarograph.

An H-cell of standard design was used with a large NaCl SCE reference electrode connected to the solution compartment by a 1 F NaF-agar salt bridge with coarse fritted disk. The potentials in Figures 36-37 are given with respect to this reference electrode which is +0.012 v. vs. SCE.

The dropping mercury electrode had a drop time of 3.60 sec. with $m^2/3t^{1/6} = 2.33$ mg. $^2/3$ sec. $^{-1/2}$.

The solutions were prepared by adding a measured amount of Cr(II) stock solution to a measured amount of descrated supporting electrolyte solution in the cell. The composition of the resulting solution was 3.65 mF Cr(II), 0.105 F HClO₄, and 0.874, 0.436, 0.0546, 0.00192, 0.00154, or 0.00106 F NaBr ($\mu = 1.00$).

Background current was measured in the deaerated supporting electrolyte solution before adding the Cr(II) solution.

Figure 37. Semi-logarithmic plot of the potential dependence of the rate of the reaction $\text{Cr}^{2^+} + \text{Br}^- \rightarrow \text{CrBr}^{2^+} + \text{e}^-$. The points are the slopes of the lines in Figure 36.

E, mv. vs. NaCI - SCE

-410

-450

-370

3. Polarographic Determination of the Rate of Reduction of CrBr²⁺.

The rate of the reduction of CrBr²⁺ was determined polarographically in 0.91 F NaBr solution. The usual quasi-reversible analysis of the polarographic wave was used (37) with the effective half-wave potential determined by the method of Koryta (38). The extrapolation to give the half-wave potential is illustrated in Figure 38.

The values of $(12t/7)^{\frac{1}{2}}\lambda$ are plotted as a function of potential in Figure 39. The minimum is close to the expected minimum required by the choice of half-wave potential, -0.501 v. vs. SCE. Similar plots were made for the same date analyzed using -0.500 v. and -0.502 v. vs. SCE for the effective half-wave potential. The fit in these cases was not as good. This gives us confidence in the choice of reference potential.

From Figure 39 we obtain $\alpha = 0.48$ and $k_h^0 = 1.82 \times 10^{-3}$ cm./sec. (referred to E = -0.500 v. vs. SCE).

Experimental details. The polarogram was obtained as described on page 100.

Chromic Bromide (K&K Laboratories) was used as the source of CrBr²⁺. Solutions were 0.91 F in NaBr, 0.066 F in HClO₄, and approximately mF in CrBr²⁺.

4. Discussion.

The values obtained for the kinetic parameters are summarized in Table 12. The standard rate constants are calculated for 1 M bromide (10⁻³ moles/cm.³). The standard potential obtained in Section 3,

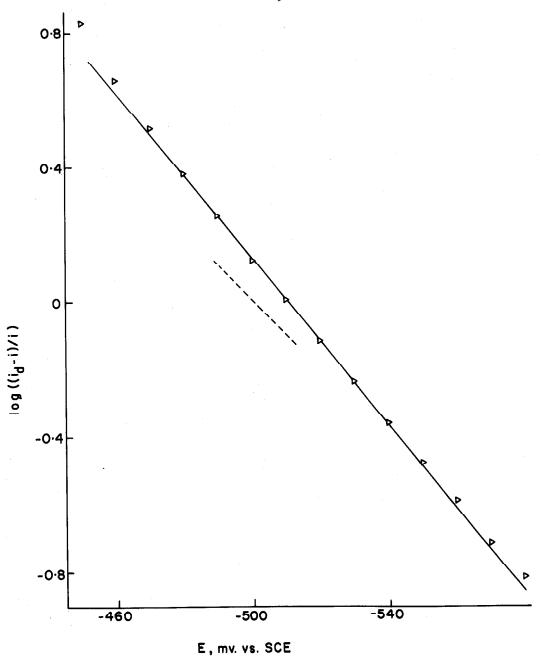


Figure 38. Nernst plot for the polarographic reduction of CrBr²⁺ in 0.91 F NaBr, 0.066 F HClO₄ solution illustrating Koryta's method of determination of the reference potential.

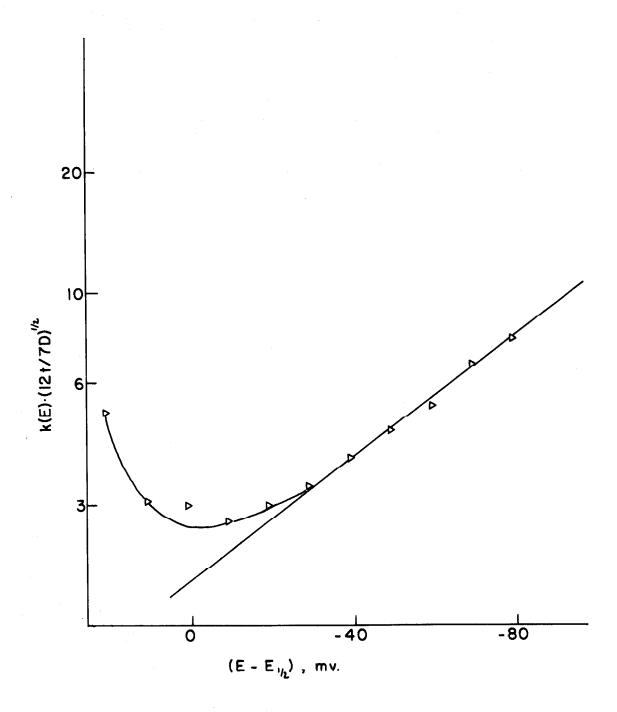


Figure 39. Semi-logarithmic plot of the potential dependence of the rate of reduction of CrBr^{2^+} from polarographic measurements. E_{1/2} is the effective half-wave potential obtained from Figure 38.

-0.501 v. vs. SCE, is shifted to -0.499 v. vs. SCE in converting from 0.91 to 1 M bromide. For convenience, the value of the standard potential has been arbitrarily chosen to be -0.500 v. vs. SCE.

The values of the standard rate constants are in remarkably good agreement. The difference in α values, though large, is not especially surprising, because of the wide variation in conditions under which the data was obtained. This point is discussed in more detail below. The derived value of the standard rate constant for Cr(II) oxidation depends much more heavily on the transfer coefficient than does the value for $CrBr^{2+}$ reduction. The agreement of the standard rate constants suggests that the α value obtained from Cr(II) oxidation is at least a well-defined quantity, though it may be far from the "true" value because of double layer effects.

TABLE 12

$k_h^0 \times 10^3$, cm./sec.	lpha Reaction	
1.82	0.21	$Cr^{2^+} + Br^- \xrightarrow{-e} CrBr^{2^+}$
1.88	0.48	$CrBr^{2+} \xrightarrow{+e^{-}} Cr^{2+} + Br^{-}$

 $E^{\circ} = -0.500 \text{ v. vs. SCE}$

IV. The Relation Between the Kinetic Parameters and Mechanism

In all of the rate determinations discussed above the effect of the ψ potential on electrode kinetics has been ignored. This is an important effect, particularly in the oxidation of Cr^{2^+} , where the reaction is strongly accelerated by negative ψ potential and strongly decelerated by positive ψ potential. Obtaining the true rates for the reactions investigated is a major project beyond the scope of this work. However, we can say a few things about the measured rate parameters.

Much valuable progress has been made in development of theory to predict electrochemical standard rate constants and their relation to homogeneous rate constants, but work in this area has been confined to adiabatic reactions (39). Even the oxidation of Cr^{2+} to Cr^{3+} is non-adiabatic, because while $Cr(H_2O)_6^{3+}$ is rigorously octahedral, $Cr(H_2O)_6^{2+}$ is highly distorted from octahedral symmetry, having two short and four long metal-oxygen bonds (40). This means that bond deformation must accompany the electron-transfer process. However, the deviation of the values of the transfer coefficient from the adiabatic value of 0.5 (41) can be speculated upon.

In analysis of kinetic data the current or some related quantity is plotted semi-logarithmically against potential. The graph should give a straight line with the slope proportional to $-\alpha$ or to $1-\alpha$, depending on whether the reaction is a reduction or an oxidation. However, if the effect of the ψ potential is taken into account, the slope must be decreased by the quantity

$$(\alpha_{n-z}) \frac{\Im}{\Re T} \frac{\partial \psi}{\partial E}$$
 (15)

independent of whether the reaction is an oxidation or a reduction (8).

This correction is often not considered to be important because the semi-logarithmic plot is linear, but quite often $\partial \psi/\partial E$ is constant or nearly so over a sufficiently wide potential range that the linearity of the plot does not mean that neglecting the ψ effect is justified.

For one-electron oxidations or reductions when the plot is linear, we have

$$\alpha_{\text{true}} = \frac{\alpha_{\text{meas}} - z \frac{\partial \psi}{\partial E}}{1 - \frac{\partial \psi}{\partial E}}$$
 (16)

where $\alpha_{\rm meas}$ is the value of α one obtains from the slope of the line if the effect of double layer is ignored. Over the potential range of interest to us the variation of ψ with potential is fairly small. We are helped in this respect by the fact that increasing the halide concentration, while shifting the flat portion of the curve to more cathodic potentials, also shifts the effective polarographic half-wave potential to more cathodic potentials, so that as one varies the halide concentration and studies the effect on the rate of oxidation of Cr(II), the effect of the double layer on the apparent value of α is remarkably constant. The actual amount of the correction on α may be as large as 0.15. With this reservation in mind, let us examine the transfer coefficients listed in Table 13.

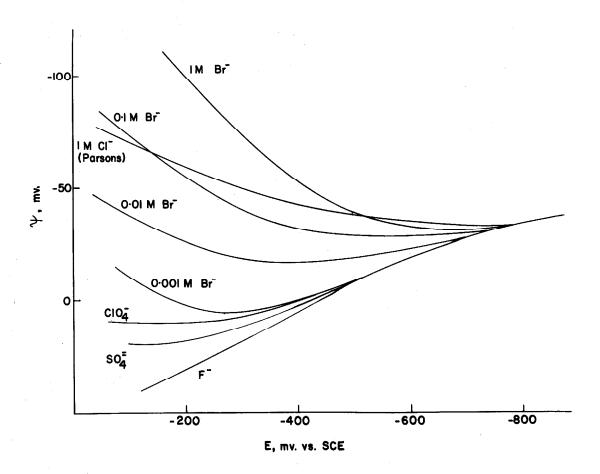


Figure 40. The ψ potential as a function of potential from the work of Gierst (42).

TABLE 13

Couple	α	Process
Cr(II)/Cr ³⁺	0,63	ox and red
CrCl ²⁺	0.43 0.49	ox red
CrBr ²⁺	0.21	OX red

The closeness of the α values for CrX^{2^+} reduction to 0.5 suggests that the electrode reaction is

$$CrX^{2^{+}} + e^{-} \longrightarrow CrX^{+}$$
 (17)

followed by a fast dissociation step

$$CrX^{+} \longrightarrow Cr^{2^{+}} + X^{-}$$
 (18)

On the other hand, the low values of the transfer coefficients obtained for the oxidation of Cr(II) to CrX²⁺ support the view that intrusion of halide into the chromium coordination sphere forms the transition state for the electron transfer rather than constituting a fast prior reaction.

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APPENDIX I

CHRONOPOTENTIOMETRY AT HANGING MERCURY DROP ELECTRODES: THE EFFECTS OF SPHERICAL DIFFUSION

Mercury pool electrodes, conventionally used in chronopotentiometry, have the disadvantage that the surface is not truly renewable.

The hanging mercury drop electrode provides an electrode surface which can be renewed in a reproducible way and is of constant area in contrast with the dropping mercury electrode.

The disadvantage of the hanging mercury drop electrode is that the solutions to the diffusion equation for common chronopotentiometric conditions are much more complicated for spherical diffusion than for linear diffusion. When the diffusion layer thickness is sufficiently small in comparison with the radius of the drop the physical situation is sufficiently close to semi-infinite linear diffusion that the simple linear solutions may be used. However, this usually demands transition times sufficiently short that switching problems become important and oscillographic recording is required.* The great advantages of avoiding instrumentation problems and being able to use more accurate and much more convenient pen and ink recorders provide ample incentive to investigate the effects of spherical diffusion at longer times.

^{*}Adequate switching is especially critical in chronopotentiometry with current reversal at short times.

Correction of the Forward Transition Time

The solution of the diffusion equation for chronopotentiometry with spherical geometry which applies to work at hanging mercury drop electrodes was first obtained by Mamantov and Delahay (1) and is a relatively easily derived and well known result. It is given in Equation 1 along with the corresponding solution to the linear problem, Equation 2, the familiar Sand equation.

$$\frac{C^{O}n\Im AD}{ir} = 1 - \exp(\lambda^{2})\operatorname{erfc}(\lambda)$$
 (1)

$$1\tau^{\frac{1}{2}} = \frac{\sqrt{\pi} \, n \, \Im \, AD^{\frac{1}{2}}C^{O}}{2} \tag{2}$$

In Equation 1, $\lambda = (D\tau)^{\frac{1}{2}}/r_0$, where r_0 is the radius of the drop. The other symbols have their usual meaning.

The qualitative effect of the change from linear to spherical diffusion is as one would predict, namely that all other things being equal, τ for Equation 1 is greater than τ for Equation 2.

If the right hand side of Equation 1 is expanded in a power series in λ , it is found that for sufficiently small values of $\lambda(\lambda \le 0.15)$ Equation 1 is well approximated by

$$i\tau^{\frac{1}{2}} \Sigma = \frac{\sqrt{\pi} \, n \, \Im \operatorname{AD}^{\frac{1}{2}} C}{2} \tag{3}$$

$$\Sigma = 1 - \frac{\pi^{\frac{1}{2}}}{2} \lambda + \frac{2\lambda^2}{3} \tag{4}$$

where

The data obtained under conditions where spherical diffusion is important can be "corrected for spherical diffusion" by multiplying the values of $i\tau^{\frac{1}{2}}$ calculated from the data by the factor Σ to obtain the Sand value for the solution in question. To facilitate the routine application of this method calculated values of Σ and the corresponding values of λ are presented in Table I-1 along with a working curve constructed from that table (Figure I-1).

It is instructive to see what the correction factor Σ is under various experimental conditions. First, for typical values $r_o = 0.06$ cm. and $D^{\frac{1}{2}} = 0.005$ cm./sec. which is a longer time than is normally used on hanging drop electrodes. Therefore, the working curve covers the region of interest. Second, let us consider the maximum time for which one should be able to avoid spherical diffusion effects. It is unreasonable to expect $i\tau^{\frac{1}{2}}$ values to be constant to better than 2%. Therefore, selecting 98% as the minimum value of Σ with the above choices of r_o and $D^{\frac{1}{2}}$, we find that τ must be less than or equal to 0.2 sec.

The upper limit for the application of the correction factor Σ is a practical one, for at longer times density gradients and other stirring effects become important. The usefulness of the correction is shown by the fact that the approximate upper limit for uncorrected transition times is roughly the lower limit for routine recording.

Although this treatment of the spherical diffusion appears beyond reproach, it is common knowledge that no correction for spherical diffusion need be made for times less than about 3-5 seconds. This is illustrated in Figures 10 and 15 above in which $i^{\frac{1}{2}}$ data corrected for

TABLE I-l Correction to $i\tau^{\frac{1}{2}}$ for Spherical Diffusion

$$i\tau^{\frac{1}{2}}\Sigma = \frac{\sqrt{\pi}}{2} \text{ n S AD}^{\frac{1}{2}}C^{0}$$

$$\text{for } \lambda = (D\tau)^{\frac{1}{2}}/r_{0} \leq 0.15$$

<u> </u>	Σ
λ 0.150 0.149 0.148 0.147 0.146 0.144 0.142 0.140 0.138 0.136 0.134 0.132 0.130 0.128 0.126 0.124 0.122 0.120 0.115 0.110 0.105 0.100 0.090 0.080	0.8821 0.8828 0.8834 0.8841 0.8848 0.8862 0.8877 0.8904 0.8918 0.8932 0.8946 0.8961 0.8961 0.8961 0.9018 0.9018 0.9032 0.9040 0.9142 0.9181 0.9256 0.9334
0,070	0.9413
0.060 0.050 0.040 0.020 0.010	0.9492 0.9574 0.9657 0.9826 0.9912
0.005	0.9956

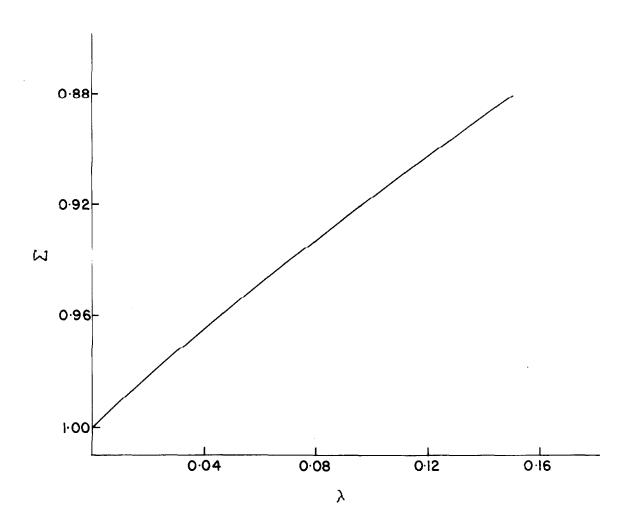


Figure 1-1. The correction factor for spherical diffusion. $i\tau^{\frac{1}{2}}\Sigma = \frac{1}{\pi^2}n\Im \Delta^{\frac{1}{2}}c^O/2; \lambda = (D\tau)^{\frac{1}{2}}/r_O.$

spherical diffusion shows a dip at times longer than about 1 sec. The uncorrected $i\tau^{\frac{1}{2}}$ values were more nearly constant. The simple explanation for this is that the experimental conditions do not correspond to the conditions of spherical diffusion for which Equation 1 was obtained.

This point is illustrated in Figure I-2 which shows the typical design of a hanging mercury drop electrode of the Kemula or Shain type:

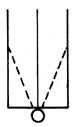


Figure I-2. Hanging mercury drop electrode.

The diffusion volume excluded by the glass capillary is sufficiently large that at intermediate times the increase in diffusion volume provided by the spherical geometry is compensated for by the excluded volume. This cancellation is fortuitous and of course highly dependent on the exact geometry.

Experimental Verification of the Spherical Correction

The reduction of Cd(II) in perchlorate solution was investigated on a hanging mercury drop electrode of the Kemula type in which the capillary end was ground to a cone as illustrated by the dotted lines in Figure I-2 in order to minimize the excluded volume effect. The

data and the calculated raw and corrected values of $i\tau^{\frac{1}{2}}$ are presented in Table I-2.

TABLE I-2

i, µa.	τ, sec.	λ	iτ ² , μα. sec. ^{1/2}	iτ ^½ Σ	, µа. sec. ²
20,08	6.14	0.1069	49.8		45.5
25.55	3.684	0.0827	48.6		45.2
33•73	2.0/16	0.0618	. 48.3		45.8
40.28	1.286	0.0508	47.4		45.4
55.18	0.732	0.0369	47.2		45.6
94.25	0.249	0.0249	47.0		45.9
				Av.	45.6+0.2
American desired to the second se	- 1		1/3 ~1/3		
-3 o \ C			፯ ~ቫ.		

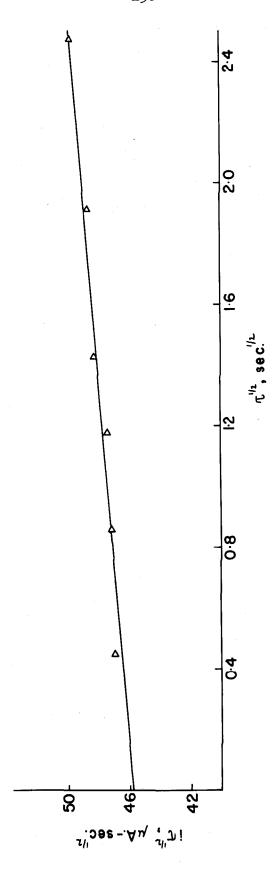
$$D^{\frac{1}{2}} = 0.00246$$
 $\pi^{\frac{1}{2}} n \Im AD^{\frac{1}{2}} C^{0}/2 = 45.5$

The agreement between the measured value (the left hand side of Equation 3) and the calculated value (the right hand side of Equation 3) is convincing evidence that application of the spherical correction factor is a reliable procedure.

Additional confirmation is given by plotting $i\tau^{\frac{1}{2}}$ as a function of $\tau^{\frac{1}{2}}$. The τ = 0 intercept should give the corrected value of $i\tau^{\frac{1}{2}}$. This is shown in Figure I-3. The intercept is 45.7.

Experimental procedure. Standard chronopotentiometric circuitry was used.

Chronopotentiometric waves at long times were recorded on a Moseley Autograph X-Y recorder; at short times they were recorded by



Transition time dependence of the it product for reduction of Cd(II) at a hanging mercury drop electrode illustrating the extrapolation to zero time which gives the Sand value intercept. Solution: 2.65 mF Cd(ClO₄)2, 76.5 mF HClO₄ (μ = 1.06). Figure I-5.

photographing the trace of a Tektronics Type 531A oscilloscope equipped with Type D Plug-in Unit.

A solution approximately 0.2 F in Cd(ClO₄)₂ was prepared by adding less than a stoichiometric amount of HClO₄ to solid CdCO₃ and filtering off the excess salt. The solution was standardized by titration with EDTA solution standardized by titrating aliquots of a standard zinc solution made from zinc metal.

Sufficient $Cd(ClO_4)_2$ stock solution was mixed with $NaClO_4/HClO_4$ supporting electrolyte solution to give a solution for chronopotentiometric investigation with 2.65 mF $Cd(ClO_4)_2$, 76.3 mF $HClO_4$ (μ = 1.06). The indicator electrode was a Kemula-type mercury hanging drop electrode modified as described above with area 0.0409 cm.² and radius 0.0571 cm. as determined from the weight of 10 drops.

Conclusions

Chronopotentiometry on hanging mercury drop electrodes at times where spherical diffusion effects are important can be accurately corrected by multiplying the values of $i\tau^{\frac{1}{2}}$ by the factor Σ obtained from the working curve in Figure I-1. The value of $i\tau^{\frac{1}{2}}\Sigma$ is equal to the value of $i\tau^{\frac{1}{2}}$ one would obtain for linear diffusion (the Sand value). In the region where the correction is most useful, significant departure from the conditions of spherical diffusion may be caused by the diffusion volume excluded by the support for the mercury drop.

Chronopotentiometry with Current Reversal:

Correction of the Transition Time Ratio

Consider a solution containing bulk concentration of the oxidized species 0 which can be electrochemically reduced to R and subsequently reoxidized to 0. Assume that the magnitude of the current is constant, but that its direction is changed at a time t_f which is less than or equal to the forward transition time for 0. The equation relating t_f , the forward time, and τ_r , the reverse transition time, is obtained by solving the differential equation

$$\frac{\partial C_0(r,t)}{\partial t} = D_0 \left[\frac{\partial^2 C_0(r,t)}{\partial r^2} + \frac{2}{r} \frac{\partial C_0(r,t)}{\partial r} \right]$$
 (5)

with the boundary and initial conditions

$$C_{O}(r,0) = C_{O}(\infty,t) = C_{O}^{O}$$

$$C_{R}(r,0) = C_{R}(\infty,t) = 0$$

$$\left(\frac{\partial C_{O}(r,t)}{\partial r}\right)_{r=r_{O}} = \frac{1}{n \Im AD}$$

$$D_{O}\left(\frac{\partial C_{O}(r,t)}{\partial r}\right)_{r=r_{O}} + D_{R}\left(\frac{\partial C_{R}(r,t)}{\partial r}\right)_{r=r_{O}} = 0$$
(6)

The subscript O refers to the oxidized species, O, the subscript R to the reduced species, R, and r_0 is the radius of the electrode.

After the change of variable

$$U(r,t) = r[C^{0} - C_{0}(r,t)]$$
 (7)

a solution is readily obtained using standard Laplace transform methods. The result is*

$$0 = 1 + experfc a \lambda - 2 experfc \lambda$$
 (8)

where

$$\lambda = \frac{D^2}{r_0} \tau^{\frac{1}{2}}$$
; $a = \left(1 + \frac{t_1}{\tau_1}\right)^{\frac{1}{2}}$ (9)

This solution has in common with the familiar solution to the corresponding problem with linear diffusion:

$$\frac{t_f}{\tau_r} = 3 \tag{10}$$

the important feature that the result is independent of C° , i, and A.

Figure I-4 shows the variation of transition time ratio with forward time according to Equation 8. $D^{\frac{1}{2}}/r_0$ is typically 0.05. Figure I-5 gives the correction to the measured ratio t_f/τ_r which must be applied to obtain the value for linear diffusion. The curve was obtained from Equation 8 by calculating a for various values of λ and using the relation $\rho = 3/(a^2-1)$. A similar curve for ρ as a function of $t_f^{\frac{1}{2}}$ is shown in Figure I-6.

If the simple model assumed by Equation 8 is obeyed, $\rho(t_f/\tau_r)$ = 3.00. If chronopotentiometry with current reversal is done on second time scales the application of the correction factor ρ to the measured transition time ratios should provide a convenient check for any unusual behavior of the system.

^{*}This result has also been obtained by Murray and Reilly (2).

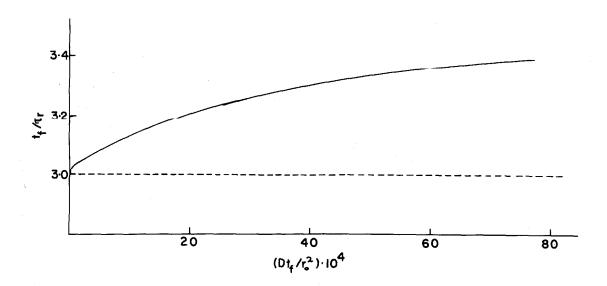


Figure I-4. Variation of the transition time ratio with forward time for spherical diffusion. Calculated from Equation 8.

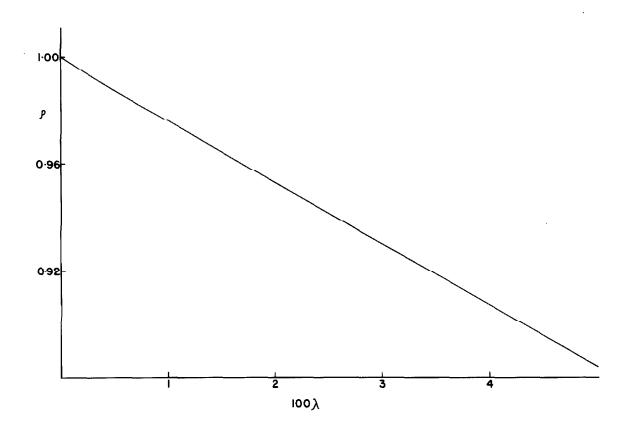


Figure I-5. Working curve for the correction factor for transition time ratios. Calculated from Equation 8.

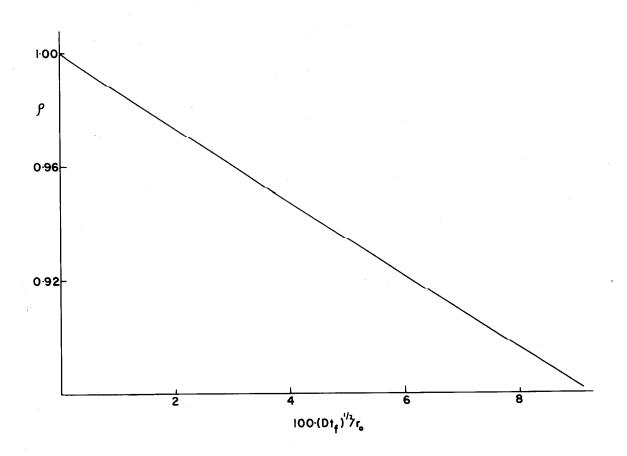


Figure I-6. Working curve for the correction factor for transition time ratios. Calculated from Equation 8.

Experimental Investigation of the Spherical Correction

The relevance of this treatment to experiment was tested by examining the reverse current chronopotentiometric behavior of Fe(II) in pyrophosphate solution at pH 2. It is known that under these conditions Fe(II) conforms to the simple behavior assumed by Equation 8 (3). A typical chronopotentiogram shown in Figure I-7 illustrates the features which make this system ideal. The large potential difference between Fe(III) oxidation and background gives an exceptionally well defined transition time, and the near reversibility of the couple minimizes the effect of double layer charging.

The results presented in Figure I-8 show that the deviation from linear behavior caused by spherical diffusion is rather small. Some data are presented in a slightly different way in Figure I-9. This shows the surprising result that the effect of spherical diffusion is highly current density dependent. Equation 8 not only predicts no current density dependence but also predicts that all the points in Figure I-9 must lie below the dotted line. Figures I-10 and I-11 show the dependence of the transition time ratio, the usual parameter of interest, on t_f and it_f, respectively. These figures make it clear that abnormally low values of the transition time ratio accompanied by severe irreproductibility are characteristic of low current densities. The same general characteristics have been observed by Gross (4). We suggest that the abnormally long reverse transition times are due to material formed during the forward time that is trapped between the mercury drop and the base of the capillary.

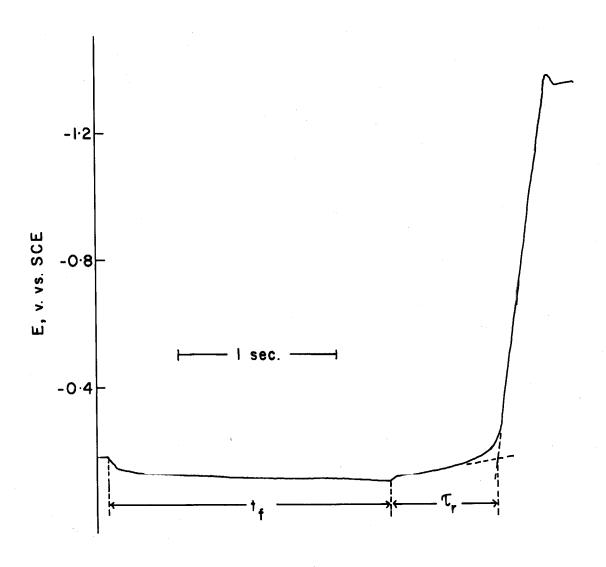


Figure I-7. Chronopotentiometric wave with current reversal for 30 mF FeSO₄ in 0.5 F Na₄P₂O₇ at pH 2.

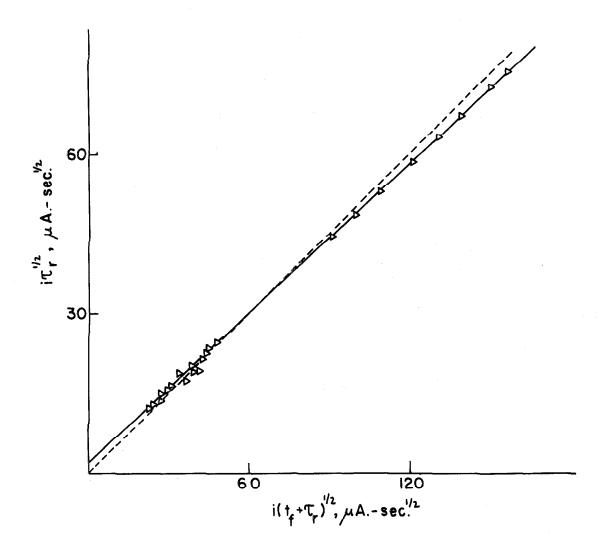


Figure I-8. The effect of spherical diffusion on transition time ratios. The dotted line shows the theoretical behavior for linear diffusion. The points were obtained as illustrated in Figure I-7.

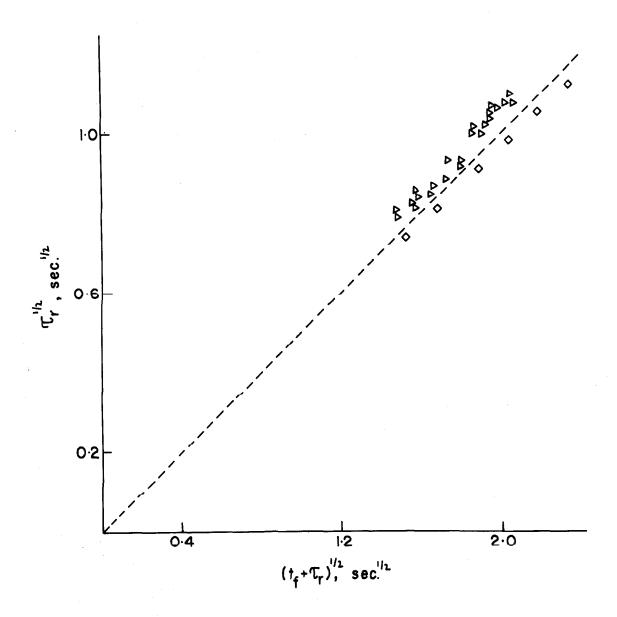


Figure I-9. Illustration on the pronounced current density dependence of the data shown in Figure I-8. The dotted line shows the theoretical behavior for linear diffusion. The points above the line were obtained at a current density of $367~\mu\text{A./cm.}^2$, those below the line at $1468~\mu\text{A./cm.}^2$

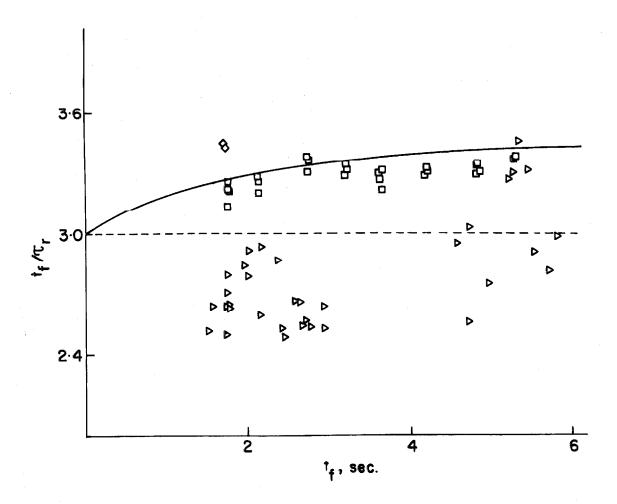


Figure I-10. Illustration of the pronounced deviation of the data of Figure I-8 from the predicted behavior for spherical diffusion, the solid line. The dotted line shows the predicted behavior for linear diffusion. , 367μA./cm.²; , 1467 μA./cm.²; , 2440 μA./cm.²

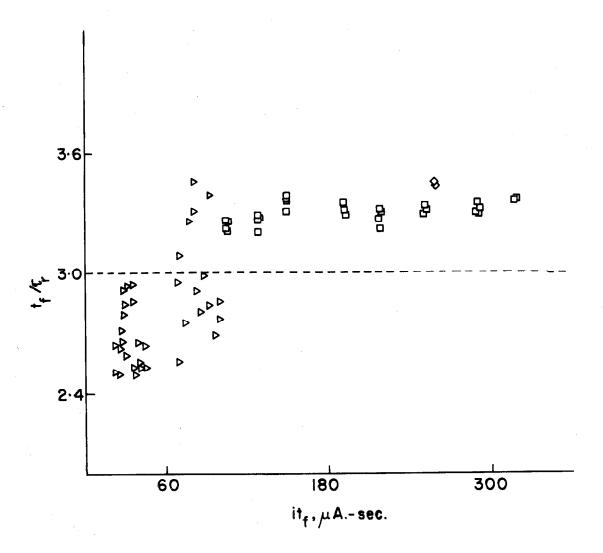


Figure I-11. The dependence of the deviation of the data of Figure I-8 from ideal behavior on it $_{\rm f}$, the number of microcoulombs of material formed during the forward time. \flat , 367 $\mu A./{\rm cm}.^2;$ \Box , 1467 $\mu A./{\rm cm}.^2;$ \Diamond , 2440 $\mu A./{\rm cm}.^2$

The most important feature of these data is their mimecry of product adsorption behavior at low current densities. At very low current densities the amount of material trapped is comparable to the total amount formed. Figure 20 illustrates the similarity of the results to those obtained with product adsorption. The "amount adsorbed" for Fe(II) in pyrophosphate at pH 2 from Figure 20 is about 150 μ C./cm.² There is ample evidence (3) that there is no product adsorption in this system.

Experimental procedures. The equipment has been described above (page 135).

Solutions of Fe(II) were prepared by dissolving the appropriate quantity of FeSO₄·7H₂O in a supporting electrolyte solution prepared by adjusting the pH of 0.5 F Na₄P₂O₇ solution to pH 2 with 18 F H₂SO₄. The final solutions were 30 mF in Fe(II).

The cathodic background wave for the small amount of Fe(III) present was measured at intervals during each experiment using a very low current density. This cathodic background wave was used to correct the measured reverse transition time by subtracting from it the appropriate value of the transition time for the measured bulk concentration of Fe(III). In no case was this correction more than 3% of the reverse transition time. It was always less than 1% for current densities greater than 100 $\mu a/cm$.²

Conclusions

He who approaches reverse current chronopotentiometry at spherical electrodes with a spherical correction factor and a prayer needs the prayer.

APPENDIX II

PARALLEL REACTIONS

Consider the electrochemical reactions

$$R \xrightarrow{n_1 e^-} O_1 \tag{1a}$$

$$R \xrightarrow{n_2 e^-} O_2 \tag{1b}$$

in which reactions (la) and (lb) are characterized by the parameters E_i^0 , α_i , k_i , and D_i , i=1,2. We wish to find the current and the charge which would flow in a potential step experiment of the following type. The solution initially contains only R and the initial potential, E_0 , is adjusted so that no current flows due to the oxidation of R. At time t=0 the potential is stepped to a value E at which R is oxidized to O_1 and O_2 . O_1 and O_2 are not in chemical equilibrium with each other.*

The current flowing for each reaction is given by (1)

$$\frac{I_{1}}{n_{1} \Im} = D_{1} \left(\frac{\partial C_{1}}{\partial x} \right)_{x=0} = -[C_{R}(0,t)\kappa_{if} - C_{1}(0,t)\kappa_{ib}], i=1,2$$
 (2)

where

$$\kappa_{if} = k_i \exp[(1-\alpha_i)^{\frac{n_i \Im}{RT}} (E-E_i^{\circ})]$$
 (3a)

$$\kappa_{ib} = k_i \exp[-\alpha_i \frac{n_i \Im}{RT} (E-E_i^{O})]$$
 (3b)

^{*}The solution to this problem was suggested by Joseph H. Christie of C.I.T.

and the other symbols have their usual meaning.

The solution to the problem is obtained by solving the diffusion equation:

$$\frac{\partial t}{\partial C} = D \frac{\partial x_S}{\partial z_C} \tag{4}$$

with the initial conditions

$$C_R(x,0) = C_R^0; \quad C_1(x,0) = 0, \quad i = 1,2$$
 (5)

and the boundary conditions

$$C_{R}(\infty,t) = C_{R}^{O}; \quad C_{i}(\infty,t) = 0, \quad i = 1,2$$
 (6a)

$$-D_{R} \left(\frac{\partial C_{R}}{\partial x} \right)_{x=0} = D_{1} \left(\frac{\partial C_{1}}{\partial x} \right)_{x=0} + D_{2} \left(\frac{\partial C_{2}}{\partial x} \right)_{x=0}$$
 (6b)

The solutions to Equation 4 in Laplace transform space are

$$\overline{C}_{i}(x,s) = \xi_{i} \exp(-s^{\frac{1}{2}}x/D_{i}^{\frac{1}{2}}), i = 1,2$$
 (7a)

$$\overline{C}_{R}(x,s) = \frac{C_{R}^{0}}{s} + \xi_{R} \exp(-s^{\frac{1}{2}}x/D_{R}^{\frac{1}{2}})$$
 (7b)

where all conditions except (6b) have been applied.

Transforming Equation 2 and combining with the derivatives of Equation 7, we find

$$\frac{\overline{I}_{i}}{n_{i} \Im} = -D_{i}^{\frac{1}{2}} s^{\frac{1}{2}} \xi_{i}, i = 1,2$$
 (8)

Combining the transform of Equation 6b with Equation 8 and solving for the constants of integration, ξ_i , i = 1,2, we obtain

$$\xi_{2} = \frac{\frac{C_{R}^{\circ}}{s} \left[\kappa_{2f} D_{1}^{\frac{1}{2}} s^{\frac{1}{2}} + \kappa_{1b} \kappa_{2f} \right]}{\left\{ \left(D_{1} D_{2} \right)^{\frac{1}{2}} s + \left[\left(\frac{D_{1} D_{2}}{D_{R}} \right)^{\frac{1}{2}} \left(\kappa_{1f} + \kappa_{2f} \right) + \kappa_{1b} D_{2}^{\frac{1}{2}} + \kappa_{2b} D_{1}^{\frac{1}{2}} \right] s^{\frac{1}{2}} + K_{2b} D_{1}^{\frac{1}{2}} s^{\frac{1}{2}} s^{\frac{1}{2}} + K_{1b} K_{2b} \right\}}$$

A similar equation is obtained for ξ_1 by permuting all of the numerical subscripts in Equation 9.

The current is obtained by finding the inverse transform for Equation 8. Equation 9 can be written in the form

$$\xi_2 = \frac{\lambda p + \mu}{(p + \gamma)(p + \beta)} \tag{10}$$

where $p = s^{\frac{1}{2}}$. From this form we find the inverse transform (2) and also the current:

$$\frac{-I_{\underline{i}}}{n_{\underline{i}}} \approx \frac{D_{\underline{i}}^{\frac{1}{2}}C_{R}^{0}}{\gamma - \beta} \left\{ (\gamma \lambda_{\underline{i}} - \mu_{\underline{i}}) \exp(\gamma^{2} t) \operatorname{erfc}(\gamma t^{\frac{1}{2}}) \right.$$

$$- (\beta \lambda_{\underline{i}} - \mu_{\underline{i}}) \exp(\beta^{2} t) \operatorname{erfc}(\beta t^{\frac{1}{2}}) \right\}, \quad i = 1, 2.$$
(11)

and by integration, the charge

$$\frac{-Q_{1}}{n_{1}} \cdot \frac{D_{1}^{\frac{1}{2}C_{R}}^{0}}{\gamma - \beta} \left(\gamma^{-2} (\gamma \lambda_{1}^{-\mu_{1}}) \left(\frac{2\gamma t^{\frac{1}{2}}}{\pi^{\frac{1}{2}}} - 1 + \exp(\gamma^{2} t) \operatorname{erfc}(\gamma t^{\frac{1}{2}}) \right) - \beta^{-2} (\beta \lambda_{1}^{-\mu_{1}})^{2} \cdot \left(\frac{2\beta t^{\frac{1}{2}}}{\pi^{\frac{1}{2}}} - 1 + \exp(\beta^{2} t) \operatorname{erfc}(\beta t^{\frac{1}{2}}) \right) \right), \quad i = 1, 2$$
(12)

where

$$\lambda_{i} = \kappa_{if} / D_{i}^{\frac{1}{2}}, i = 1,2$$
 (13a)

$$\mu_{i} = \frac{\kappa_{if} \kappa_{jb}}{(D_{i}D_{j})^{\frac{1}{2}}}, i = 1,2; j = 1,2, \text{ not } i$$
(15b)

$$\gamma = \frac{1}{2} (e - \sqrt{e^2 - 4f}) , \beta = \frac{1}{2} (e + \sqrt{e^2 - 4f})$$
 (13c)

$$e = (\kappa_{1f} + \kappa_{2f}) / D_{R}^{\frac{1}{2}} + \kappa_{1b} / D_{1}^{\frac{1}{2}} + \kappa_{2b} / D_{2}^{\frac{1}{2}}$$
 (13d)

$$f = \kappa_{1f} \kappa_{2b} / (D_2 D_R)^{\frac{1}{2}} + \kappa_{1b} \kappa_{2f} / (D_1 D_R)^{\frac{1}{2}} + \kappa_{1b} \kappa_{2b} / (D_1 D_2)^{\frac{1}{2}}$$
 (13e)

The solution for the charge, Equation 12, is sufficiently complicated that the qualitative results are obscured by the algebra. In particular, the parameters γ and β contain all of the rate parameters for both reaction paths, which means that one cannot single out terms corresponding to a single path.

When the arguments of the error function complement are sufficiently small, an expansion of these functions shows that when $\beta t^{\frac{1}{2}} \leq$ 0.01, then the charge going to each reaction is proportional to the rate for that reaction, so that

$$\frac{Q_{1}}{Q_{1}+Q_{2}} = \frac{\kappa_{1f}}{\kappa_{1f}+\kappa_{2f}} \quad \text{whenever } \beta t^{\frac{1}{2}} \leq 0.01 \quad (14)$$

Intuitively this means that if the reactions are sufficiently slow, then the backward reactions have no effect and the amount of current going to each reaction is affected only by the competition between the two reaction paths.

If γ is sufficiently small that a small argument expansion may be used for the error function complement of $\gamma^{\frac{1}{2}}$ but at the same time β is sufficiently large that a large argument expansion may be used for the error function complement of $\beta t^{\frac{1}{2}}$, it can be shown that the same relationship holds for the product ratios:

$$\frac{Q_{1}}{Q_{1}+Q_{2}} = \frac{\kappa_{1f}}{\kappa_{1f}+\kappa_{2f}} \quad \text{whenever} \quad \beta t^{\frac{1}{2}} > 5, \ \beta \gg t^{\frac{1}{2}}, \ E - E_{1}^{\circ} \geqslant 0.2 \text{ v.}$$

$$\tag{15}$$

Here the physical condition is that the reaction is quasi-reversible, but the potential is far enough from the nearest standard potential that the back reactions need not be considered. Of course under these conditions

$$Q_1 + Q_2 \cong \frac{2n \Im D^{\frac{1}{2}} A C_R^{O_1 \frac{1}{2}}}{\sqrt{\pi}}$$
 if $n_1 = n_2 = n$ (16)

The relation

$$\frac{Q_1}{Q_1 + Q_2} = \frac{\kappa_{1f}}{\kappa_{1f} + \kappa_{2f}} \tag{17}$$

also holds under a wide variety of conditions excluded in Equations $1^{1/4}$ and 15. This is readily demonstrated by calculating the values of Q_1 and Q_2 directly and comparing the value of $Q_1/(Q_1+Q_2)$ with the calculated rate ratio, $\kappa_{1f}/(\kappa_{1f}+\kappa_{2f})$. However, it is not possible to obtain a simple algebraic condition to insure that the relationship holds as is the case for Equations $1^{1/4}$ and 15.

The results of calculation of the ratios directly from the equation suggest that if the standard rate constants do not differ by more than a factor of about 5 and if the product $(1-\alpha_i)(E-E_i^0)n_i$ is greater than about 0.100 v., then Equation 17 should hold. However,

for cases in which the conditions of neither Equation 14 nor Equation 15 apply, the safest approach is to calculate the charge ratios directly from Equation 12.

APPENDIX III

REVERSE CURRENT CHRONOPOTENTIOMETRY: REVERSAL AFTER THE TRANSITION TIME

Consider reverse current chronopotentiometry in a solution containing bulk concentrations $C_1^{\ 0}$ and $C_2^{\ 0}$ of the species O_1 and O_2 , respectively, with the reactions:

$$O_1 + n_1 e \longrightarrow R_1; \qquad O_2 + n_2 e \longrightarrow R_2$$
 (1)

Suppose that O_2 is reduced at more cathodic potentials than is O_1 , and that the couple O_2/R_2 is sufficiently irreversible that R_2 is oxidized at more anodic potentials than is R_1 . If one were to reverse the current on the wave for O_2 reduction, the expected qualitative potential-time behavior is as illustrated in Figure III-1.

This situation is easily obtainable in practice, for instance, with many choices for O_1 on mercury electrodes where O_2 is H^+ or H_2O and R_2 is H_2 .

The solution to this problem which expresses the relationship of the reverse time, τ_3 , to the forward times, τ_1 and t_2 , is obtained by solving the diffusion equation for semi-infinite linear diffusion for the concentration of R_1 as a function of x, the distance from the electrode, and t, the time from τ_1 , and applying the condition that (1)

$$C_{R_1}(x=0, t=\tau_3) = 0$$

In the following derivation all diffusion coefficients are assumed to be equal and C_{R_1} (x,t) \equiv C(x,t). Also, $n_1=n_2$. The problem, then, is

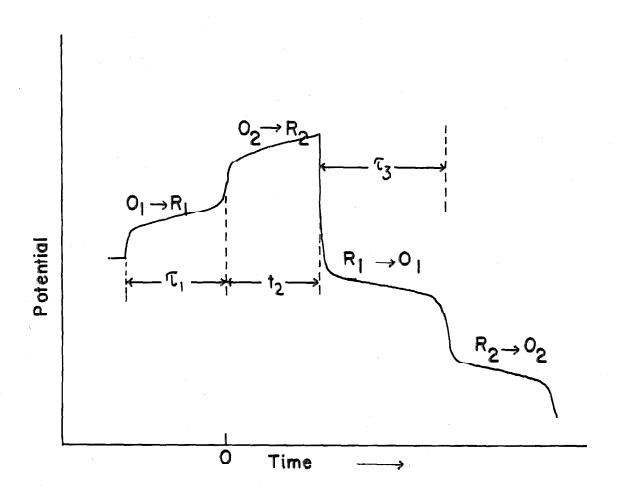


Figure III-1. Qualitative behavior for reverse current chronopotentiometry with reversal after the transition time. Case in which the product of the second reduction is electronactive at potentials where the product of the first is reoxidized.

simply to solve the differential equation

$$\frac{\partial c(x,t)}{\partial t} = D \frac{\partial^2 c(x_1 t)}{\partial x^2}$$
 (2)

subject to the initial condition

$$C(x,0) - C_{0_1}^0 e^{-x^2/4D\tau_1} - \frac{1}{n \Im AD} \times \operatorname{erfc}\left(\frac{x}{2D^2 \tau_1^{\frac{1}{2}}}\right)$$
 (3)

and the boundary conditions (1)

$$C(\infty,t) = 0 (4a)$$

$$\frac{\partial C(x,t)}{\partial x}\Big|_{X=0} = \begin{cases} -\frac{1}{nNAD} \left[\frac{1}{2} + \frac{1}{\pi} \sin^{-1} \left(\frac{\tau_1 - t}{\tau_1 + t} \right) \right]; & 0 \le t \le t_2 \\ +\frac{1}{nSAD} & ; & t_2 \le t \end{cases}$$

$$(4b)$$

The Laplace transform of Equation 2 is

$$C(x,0) + s \overline{C}(x,s) = D \frac{\partial^2 \overline{C}(x,s)}{\partial x^2}$$
 (5)

where s is the transform variable. The solution to this equation is obtained using the method of variation of parameters assuming a solution of the form $v(x) \exp(-s^{\frac{1}{2}}x/D^{\frac{1}{2}})$. The general solution to the complete equation is

$$\overline{C}(x,s) = \beta e^{-s^{\frac{1}{2}}x/D^{\frac{1}{2}}} + \xi e^{s^{\frac{1}{2}}x/D^{\frac{1}{2}}}$$
 (6)

$$-\frac{\mathbf{i}}{n\Im\operatorname{AD}}\frac{x}{s}\operatorname{erfc}\left(\frac{x}{2D^{\overline{2}}\tau_{1}^{\overline{2}}}\right)+\frac{2\mathbf{i}\tau_{1}^{\overline{2}}}{n\Im\operatorname{AD}^{\overline{2}}\pi^{\overline{2}}s}\operatorname{e}^{-x^{2}/4D\tau_{1}}$$

$$+\frac{\mathrm{i}}{2\mathrm{n}\,\mathrm{SAD}^{\frac{1}{2}\mathrm{S}^{\frac{3}{2}}}}\,\mathrm{e}^{\mathrm{S}\mathsf{T}_{\mathbf{1}}}\!\!\left[\!\mathrm{e}^{-\mathrm{s}^{\frac{1}{2}}\!\mathrm{x}/\mathrm{D}^{\frac{1}{2}}}\!\!\mathrm{erf}\!\left(\!\frac{\mathrm{x}}{2\mathrm{D}^{\overline{\mathbf{z}}}\mathsf{\tau}_{\mathbf{1}}^{\frac{1}{2}}}\!-\,\mathrm{s}^{\frac{1}{2}}\mathsf{\tau}_{\mathbf{1}}^{\frac{1}{2}}\!\right)\!-\,\mathrm{e}^{\mathrm{s}^{\frac{1}{2}}\!\mathrm{x}/\mathrm{D}^{\frac{1}{2}}}\!\!\mathrm{erf}\!\left(\!\frac{\mathrm{x}}{2\mathrm{D}^{\overline{\mathbf{z}}}\mathsf{\tau}_{\mathbf{1}}^{\frac{1}{2}}}\!+\!\mathrm{s}^{\frac{1}{2}}\mathsf{\tau}_{\mathbf{1}}^{\frac{1}{2}}\!\right)\!\right]$$

The transformed boundary conditions are

$$\overline{C}(\infty, s) = 0 \tag{7a}$$

$$\frac{n\Im\operatorname{AD}\left(\frac{\partial\overline{C}(x,s)}{\partial x}\right)_{x=0}}{i} = \frac{3}{2s} e^{-st_2} - \frac{1}{s} + \frac{e^{-st_2}}{s\pi} \sin^{-1}\left(\frac{\tau_1 - t_2}{\tau_1 + t_2}\right) \tag{7b}$$

$$+ \frac{\sqrt{2} t_{2}^{\frac{1}{2}} \tau_{1}^{\frac{1}{2}}}{s} e^{-st_{2}/2} \sum_{k=1}^{n} \frac{1}{n} \frac{e^{-st_{2}x_{k}/2(1-x_{k})^{\frac{1}{2}}}}{(2\tau_{1}+t_{2}+t_{2}x_{k})}$$

where

$$x_{k} = \cos(\pi(2k-1)/2n)$$
 (8)

The sum in Equation 7b arises from a quadrature approximation (2) of the integral

$$\int_{0}^{t_{2}} \frac{e^{-st}}{t^{2}(\tau_{1}+t)} dt \tag{9}$$

which is a form of Smith's integral (3).

Appropriate combination of 6, 7a, and 7b gives the solution in transform space evaluated at x=0

$$\overline{C}(0,s) = \frac{-i}{n \Im AD^{\frac{1}{2}} s^{\frac{3}{2}}} \left[\left(\frac{3}{2} + \frac{1}{\pi} \sin^{-1} \left(\frac{\tau_1 - t_2}{\tau_1 + t_2} \right) \right) e^{-st_2} \right]$$

$$+\sqrt{2} t_{2}^{\frac{1}{2}} \tau_{1}^{\frac{1}{2}} \sum_{k=1}^{n} \frac{1}{n} \frac{e^{-st_{2}(1+x_{k})/2}(1-x_{k})^{\frac{1}{2}}}{(2\tau_{1}+t_{2}+t_{2}x_{k})}$$
(10)

$$- e^{ST_1} \operatorname{erfc}(s^{\frac{1}{2}} \tau_1^{\frac{1}{2}}) - \frac{2 s^{\frac{1}{2}} \tau_1^{\frac{1}{2}}}{\pi^{\frac{1}{2}}}$$

The inverse transform of this expression involves the integral

$$\int_{0}^{t_{2}} \frac{(t-\alpha)^{\frac{1}{2}} d\alpha}{(\alpha+\tau_{\perp})\alpha^{\frac{1}{2}}} \tag{11}$$

which is also evaluated by quadrature approximation (2). Application of the condition $C(0,t_2+\tau_3)=0$ to the transformed equation gives the final solution

$$\left(\frac{\tau_{3}}{\tau_{1}}\right)^{\frac{1}{2}} = \frac{1 + \frac{1}{n} \sum_{i=1}^{n} \frac{(1 - y_{i})}{\left[1 + y_{i} + \frac{2\tau_{1}}{t_{2} + \tau_{3}}\right]} - \frac{1}{m} \sum_{j=1}^{m} \frac{(1 - x_{j})^{\frac{1}{2}} \left(\frac{2\tau_{3}}{\tau_{2}} + 1 - x_{j}\right)^{\frac{1}{2}}}{\left[\frac{2\tau_{1}}{t_{2}} + 1 + x_{j}\right]}}{\frac{3}{2} + \frac{1}{\pi} \sin^{-1} \left(\frac{\tau_{1} - t_{2}}{\tau_{1} + t_{2}}\right)}$$
(12)

where
$$y_{\mathbf{j}} = \cos \frac{\pi}{2} \left(\frac{2\mathbf{j} - 1}{\mathbf{n}} \right); \quad x_{\mathbf{j}} = \cos \frac{\pi}{2} \left(\frac{2\mathbf{j} - 1}{\mathbf{m}} \right)$$
 (13)

The choice n=m=5 gives sufficient accuracy for calculation. No algebraic simplification is gained by choosing n=m and combining the two sums.

As t_2 approaches infinity the two sums in the numerator of the right hand side of Equation 12 approach each other and the denominator approaches unity. Therefore

$$\lim_{t_2 \to \infty} (\tau_3/\tau_1) = 1 \tag{14}$$

This simply means that an infinite amount of R_1 would be generated during time t_2 , a trivial limiting case.

If t2 is small, Equation 12 can be approximated by

$$2\left(\frac{\tau_3}{\tau_1}\right)^{\frac{1}{2}} = 1 + \frac{1}{n} \sum_{i=1}^{n} \frac{(1 - y_i)}{\left(\frac{2\tau_1}{\tau_3} + 1 + y_i\right)}$$
 (15)

If we let $\tau_3/\tau_1=1/3$ in the right hand side of Equation 15 we can easily calculate the value of τ_3/τ_1 using

$$2\left(\frac{\tau_{3}}{\tau_{1}}\right)^{\frac{1}{2}} = 1 + \frac{1}{n} \sum_{i=1}^{n} \frac{(1 - y_{i})}{(7 + y_{i})}$$
 (16)

From Equation 16 for $n \ge 2$ we obtain $\tau_3/\tau_1 = 0.333$, the value predicted by the simple theory for the case of reversal before the transition time.

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